# Electrochemical Performance of Activated Carbon Derived from Treated Food-Waste 

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This work reports on the physical characteristics and electrochemical properties of the carbon derived from treated food-waste as electrode material. The eco-green carbon was produced by means of chemical activation using phosphoric acid as activating agent with varies activation temperature, 500 ${ }^{\circ} \mathrm{C}, 600{ }^{\circ} \mathrm{C}$ and $700{ }^{\circ} \mathrm{C}$. Highest specific surface area of $535.80 \mathrm{~m}^{2} \mathrm{~g}^{-1}$ was achieved and consists mainly of mesoporous. Field Emission Scanning Electron Microscopy images illustrated the morphology of the activated carbon was porous and homogenously distributed. The electrochemical properties of activated carbon electrodes were analyzed using cyclic voltammetry, galvanostatic charge-discharge and electrochemical impedance spectroscopy in KOH as electrolyte. The specific capacitance from cyclic voltammetry and galvanostatic charge-discharge showed $85 \mathrm{Fg}^{-1}$ and $106 \mathrm{Fg}^{-1}$. Results demonstrated that the carbon produced from treated food-waste was a promising electrode material for supercapacitor.

Keywords: food-waste, activated carbon, supercapacitor, cyclic voltammetry, specific capacitance

## 1. INTRODUCTION

An electrochemical double-layer supercapacitor (EDLC) is a device that consists ideally of a pair of polarizable electrodes [1], by storing energy through charge separation or non-faradic reaction, with the build-up of a double layer between electrode/electrolyte interfaces. EDLC is a promising alternative approach, which fulfils the gap between capacitor and battery or fuel cell. The life time of a battery or fuel cell is enhanced by the incorporation of a supercapacitor, whose characteristics of a highly reversible charge-storage process and a long-cycle life have attracted great attention, either from
researchers or from industry, as an energy storage device for electric plant. Its application has range from memory backup to hybrid electric vehicles and industrial power management [2].

Generally, in EDLC assembly, carbon materials, such as activated carbon, carbon aerogel and carbon nanotubes are used, as a result of their unique characteristics. Many researchers have chosen activated carbon (AC) over the other two carbons, owing mainly to its relatively low cost, accessibility, ease of production, reasonable surface area value, chemical stability and ability to withstand wide range of temperatures [3]. There are number of reports stating that the production of activated AC from agricultural wastes, such as coconut [4], rice husk [5], bamboo [6], waste tea [7] etc. and its effectiveness in different applications. The synthesized AC can be utilized in a wide range of applications; for instance, as an adsorbent, for colour removal and purification, and also as an electrode for batteries as shown in Table 1.

Table 1. Activated carbon derived from agricultural waste and its applications

| Raw material | $\mathbf{S}_{\text {BET }}\left(\mathbf{m}^{2} / \mathbf{g}\right)$ | Application | Reference |
| :--- | :---: | :--- | :---: |
| Oil palm empty fruit <br> bunches | - | Phenol Adsorption | $[8]$ |
| Biomass: Grass cutting, <br> horse manure, beer waste, <br> bio-sludge | 841,749, <br> 622,489 | Adsorbents for $\mathrm{CO}_{2}$ | $[9]$ |
| Industrial sludge | - | Methylene blue removal | $[10]$ |
| Coir Pith | 315 | Trichloroethlyene removal | $[11]$ |
| Sugarcane Baggase | - | Sugar decolorisation | $[12]$ |
| Walnut shells | 1800 | Methylene blue removal | $[13]$ |
| Waste tea-leaves, straw <br> based | $2245-2841$, <br> 2316 | EDLC application | $[14],[15]$ |
| Spent tea waste | - | Purification of biodiesel | $[16]$ |
| Hard shell of apricot stones | 1078 | Adsorbent for the gold <br> separation from gold- <br> plating wastewater | $[17]$ |
| Pecan shell | Treatment of chemical <br> oxygen demand (COD) | $[18]$ |  |
| Sawdust (pinewood) | 1350 | Recovery of activator | $[19]$ |
| Maize tassel | $5-1214$ | Removal of heavy metals <br> in water | $[20]$ |

This approach is more popular than using non-renewable fossil fuel, owing to the large volume of agricultural waste available. On the other hand, food-waste which is also abundant provides an alternative as AC precursor. This waste can be treated by vermicomposting as by means of this method, organic materials can be degraded homogeneously with the presence of earthworms to destroy pathogenic microorganisms and resulting in a hygienic, porous microstructure end-product [21]. This technique can be carried out using other organic waste either from municipal solid waste, agricultural
waste or even animals' manure. More importantly, this treatment can reduce waste volume by 40 to 60 $\%$ with feasible construction, low cost and low greenhouse gases emission [22].

In this work, we focus on the carbon preparation as an electrode material in a supercapacitor, using treated food-waste by vermicomposting as precursor, via the method of chemical activation. The carbonized precursor was activated at temperatures of $500^{\circ} \mathrm{C}, 600^{\circ} \mathrm{C}$ and $700^{\circ} \mathrm{C}$. The electrochemical performance of prepared carbon electrode was determined using cyclic voltammetry, and electrochemical impedance spectroscopy. To the authors' knowledge, there is yet available report on utilizing food-waste vermicompost as AC source for supercapacitor application currently. Thus, this study will diverse the application of vermicompost product not only provides waste management option but also contribution to the power sources.

## 2. METHODOLOGY

### 2.1 Carbonaceous Material Preparation

Local treated food-waste via vermicomposting was used as precursor and further dried in an oven at $110^{\circ} \mathrm{C}$ for 48 hours. 10 g of dried vermicompost was impregnated with 400 mL of $1 \mathrm{M} \mathrm{H}_{3} \mathrm{PO}_{4}$ ( $\mathrm{R} \& \mathrm{M}$ Chemicals) as the activating agent, and stirred continuously for 24 hours. The impregnated sample was then dried at $100^{\circ} \mathrm{C}$ and crushed into powder. The powder was pyrolyzed at $400^{\circ} \mathrm{C}$, and subsequently, activated at different temperatures, such as $500^{\circ} \mathrm{C}$ (FW500), $600^{\circ} \mathrm{C}$ (FW600) and 700 ${ }^{\circ} \mathrm{C}$ (FW700) at a heating rate of $10{ }^{\circ} \mathrm{Cmin}^{-1}$ for 1 hour holding time, respectively, under nitrogen flow of $1 \mathrm{Lmin}^{-1}$. The sample was cooled down inside the furnace under nitrogen flow, followed by washing with 0.5 M HCl and distilled water, to remove residual chemical and ash then dried at $110{ }^{\circ} \mathrm{C}$.

### 2.2 Physical Characteristics

Thermogravimetric analysis (TGA) measurements were carried out using TA Instruments Q500 Thermogravimetric Analyzer. Each sample about 10 mg was put onto a platinum pan and further heated from room temperature to $900{ }^{\circ} \mathrm{C}$ at the heating rate of $10^{\circ} \mathrm{C} \mathrm{min}{ }^{-1}$ via Hi-Res technique in nitrogen atmosphere. TG and DTG curves were analysed using TA Universal Analysis. The specific surface area and the pore parameters of the ACs were determined by nitrogen adsorption at 77 K , with Micromeritics ASAP 2020. The specific surface area was calculated by the conventional Brunauer-Emmet-Teller (BET) method. The pore size distributions of micropores and mesopores were evaluated based on the Barrett-Joyner-Halenda (BJH) method. A Field Emission-Scanning Microscope Electron (FESEM) - JOEL-JSM-7600F - was used to study the surface structure and pore development. XRD pattern of activated carbon was collected using D8 Advance X-Ray Diffractometer- Bruker AXS at 40 kV and 40 mA under ambient temperature ( $\mathrm{Cu} \mathrm{K} \alpha$ monochromatized radiation) at step size $0.02^{\circ}$ and step time 1s. The surface functional group of the sample was analyzed by ATR-FTIR using a Thermo Scientific Nicolet iS10 FT-IR Spectrometer equipped with ATR internal reflection system.

The IR spectrum was obtained under the resolution of $4 \mathrm{~cm}^{-1}$ over the range of $4000-550 \mathrm{~cm}^{-1}$. Each spectrum runs 32 scans in 2 s with correction against the background spectrum of air.

### 2.3 Electrochemical Measurements

A mixture of $0.9 \mathrm{~g} \mathrm{AC}, 0.05 \mathrm{~g}$ super P and 0.05 g polyvinylidene difluoride (Pvdf) (Sigma Aldrich) in N-Methyl-2-pyrrolidone (NMP) was used for electrode preparation. The $2 \mathrm{~cm}^{2}$ nickel foam was pasted with carbon slurry, and dried in the furnace at $100^{\circ} \mathrm{C}$ for four hours. Dried nickel foam was pressed at 100 kPa . A three-electrode set-up was carried out with carbon electrode, Pt and $\mathrm{Ag} / \mathrm{AgCl}$ acted as working, counter and reference electrode in 6 M KOH . Cyclic voltammetry (CV), galvanostatic charge-discharge (CD) and electrochemical impedance spectroscopy (EIS) were recorded using an Autolab electrochemical measurement unit (PGSTAT30, Germany). CV was carried out in the voltage range of -0.9 V to -0.3 V , at various scan rates $\left(1,3,5,7,9,10,30,50,70\right.$ and $\left.100 \mathrm{mVs}^{-1}\right)$. The EIS measurement was performed within a frequency range of 0.1 Hz to 10 kHz , with alternating current amplitude of 10 mV . CD measurements were conducted from -0.9 V to -0.3 V , at the current of 1 mA . Specific capacitance ( $\mathrm{Cs}, \mathrm{Fg}^{-1}$ ) were evaluated from CV curves (1) and CD (2), according to the equations below:

Specific capacitance (Cs) $=\Delta \mathrm{i} /\left(\mathrm{M}_{\mathrm{ac}} \times \mathrm{s}\right)$
Specific capacitance $(\mathrm{Cs})=(\mathrm{I} \times \Delta \mathrm{t}) /\left(\Delta \mathrm{V} \times \mathrm{M}_{\mathrm{ac}}\right)$
where $\Delta \mathrm{i}$ is average of discharge current, $\mathrm{M}_{\mathrm{ac}}(\mathrm{g})$ is the mass of active material, $\mathrm{s}\left(\mathrm{mVs}^{-1}\right)$ is the scan rate, I (A) is the discharge current, $\Delta \mathrm{t}(\mathrm{s})$ is the discharge time and $\Delta \mathrm{V}(\mathrm{V})$ represents the voltage change after a full charge or discharge.

## 3. RESULTS AND DISCUSSION

### 3.1 Physical Characteristics



Figure 1. TG and DTG curves of food waste based vermicompost

In Figure 1, thermogravimetric (TG) of the food waste based vermicompost depicted the mass loss during the pyrolysis process is divided into two phases. It can be seen that great dropped mass of $58 \%$ is observed at the early stage of the heating process. In DTG curve, first significant sharp peak is shown at $37{ }^{\circ} \mathrm{C}$, mainly due to the loss of its high water content. Another small hump can be observed in both TG and DTG curves at $293{ }^{\circ} \mathrm{C}$. This might be due to the breakdown of cellulose and hemicellulose [23,24] in the vermicompost. Arising temperature after $400^{\circ} \mathrm{C}$ showing in both DTG and TG curve implying the decomposition process is occurred.

The activation temperature of materials has an important influence on the textural properties, as tabulated in Table 2.

Table 2. Textural properties of prepared activated carbon

| Sample | Carbon <br> Yield <br> $(\%)$ | BET <br> $\left(\mathrm{m}^{2} \mathrm{~g}^{-1}\right)$ | $t$-plot <br> Micropore <br> Volume <br> $\left(\mathrm{cm}^{3} \mathrm{~g}^{-1}\right)$ | Mesopore <br> Volume <br> $\left(\mathrm{cm}^{3} \mathrm{~g}^{-1}\right)$ | Total <br> Pores <br> Volume <br> $\left(\mathrm{cm}^{3} \mathrm{~g}^{-1}\right)$ | Average <br> Pores <br> Width <br> $(\mathrm{nm})$ |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| FW500 | 41.55 | 535.80 | 0.068 | 0.18 | 0.248 | 3.7 |
| FW600 | 30.50 | 312.68 | 0.051 | 0.074 | 0.125 | 4.1 |
| FW700 | 29.26 | 173.51 | 0.012 | 0.089 | 0.101 | 4.5 |

In Table 2, it is clearly shown that $\mathrm{S}_{\mathrm{BET}}$ and total pore volume are inversely proportionate to the activation temperature. The $\mathrm{S}_{\mathrm{BET}}$ and total pore volume values decreased when the activation temperature was increased from $500{ }^{\circ} \mathrm{C}$ to $600^{\circ} \mathrm{C}$ and $700{ }^{\circ} \mathrm{C}$. The used of $\mathrm{H}_{3} \mathrm{PO}_{4}$ as an activating agent will lead to the shrinkage of the carbon structure, at temperatures above $600^{\circ} \mathrm{C}$, and results in the decrease of surface area and pore volume [25]. Figures 2(a) show the adsorption-desorption isotherm plots which explain further the information on the porosities of the AC. According to International Union of Pure and Applied Chemistry (IUPAC) classification, FW500 to FW700 showed the mixture of type I initial part and type II end part. FW500 and FW600 showed a steep isotherm at relatively low pressure $\mathrm{p} / \mathrm{p}^{\circ} \approx 0$ indicating high uptake of micropore filling. In this isotherm, we also observed that although it showed type I, but it micropore filling happened at a comparatively higher relative pressure indicating wider micropores termed as supermicroporous materials. Besides that, no long plateau is observed at middle relative pressure but an inflection point indicating the beginning of multilayer adsorption. This is mainly due to the existing of mesopores or macropores. The increase of the pyrolysis temperature from $600{ }^{\circ} \mathrm{C}$ to $700{ }^{\circ} \mathrm{C}$ has reduced the micropore as can be seen that the steepness at low relative pressure is reducing. The majority of the carbon prepared in this study is mainly mesoporous, as approximately $72 \%$ of $\mathrm{V}_{\text {meso }}$ is shown in FW500. This statement can be confirmed by analysing pore size distribution, using BJH theory in Figure 2(b). It can be seen that the pore distribution is mainly focusing at about 3-4 nm where the highest peak is observed indicating the existence of mesopore structure is in accordance to the
hysteresis loop as Figure 2(a). The second peak of increment pore volume is noted at the range of 6-9 nm , however, the peak is gradually disappeared as the activation temperature increased.


Figure 2. (a) Adsorption-desorption isotherm and (b) BJH pore size distributions of FW500, FW600, and FW700

Figure 3 presents the micrographs for all types of FW activated carbon prepared from a variety of activation temperatures. Micrographs were recorded with 200,000x magnification. Pores of heterogeneous shapes and sizes were observed from different activation temperatures. It can be seen that FW500 produced small pores and distributed homogenously. At $600^{\circ} \mathrm{C}$, small pores with distinct size within the bigger pores are developed, while in FW700 porosity was reduced and left only larger pores in the carbon, as can be seen in Figure 3(c). This is one of the reasons contributed to low surface area in FW700 as surface area is inversely proportionate to the pore size. The FESEM images shown matched with the textural properties explained.


Figure 3. Porosity images observed from FESEM (a) FW500; (b) FW600 and (c) FW700

The EDX result has proven that FW is successfully converted to activated carbon in which it occupied highest percentage in carbon element compared to other elements as shown in Figure 4.

In the Figure 5, the characteristic peak of carbon can be detected at the angle $2 \theta$ of $26.6^{\circ}$ [006], however, it does not show broad peak which supposed to be similar with the XRD pattern of typical activated carbon. This is mainly due to the crystalline substance i.e. quartz which detected at $2 \theta=$ $20.8^{\circ}[100]$ and $2 \theta=26.6^{\circ}[101]$ which cannot be eliminated even at high temperature.


Figure 4. EDX of prepared FW-based carbon


Figure 5. X-ray diffraction pattern of FW activated carbons with various activation temperatures

Based on the IR spectrum, raw FW showed peak $3328 \mathrm{~cm}^{-1}$ which is assigned to $\mathrm{O}-\mathrm{H}$ stretching of hydroxyl group. Peak of $1582 \mathrm{~cm}^{-1}$ and $1643 \mathrm{~cm}^{-1}$ can be observed which is attributed to the $\mathrm{N}-\mathrm{H}$ plane of amides II and $\mathrm{C}=\mathrm{O}$ of amides I and carboxylates. The broad peak of $1386 \mathrm{~cm}^{-1}$ appeared to be $\mathrm{O}-\mathrm{H}$ bending of phenol and the shoulder peak which can be observed at $1082 \mathrm{~cm}^{-1}$ is due to the quartz element while the sharp peak at $1025 \mathrm{~cm}^{-1}$ is assigned to $\mathrm{Si}-\mathrm{O}$ or $\mathrm{Si}-\mathrm{O}-\mathrm{Si}$ stretching of clay minerals and silica. After the raw FW is soaked with phosphoric acid, it can be seen that the O-H peak is broaden indicating phosphoric acid acts as dehydrating agent material [26]. In addition, a new peak
appeared at $2338 \mathrm{~cm}^{-1}$ is attributed to the phosphate compound. The peak of $1706 \mathrm{~cm}^{-1}$ suggests the stretching vibration of $\mathrm{C}=\mathrm{O}$ in ketones, aldehydes, carboxylic acids or acid phosphate esters indicating the reaction of phosphoric acid with raw material.


Figure 6. FT-IR spectrum of raw and soaked FW, FW500, FW600 and FW700

The peak of $1616 \mathrm{~cm}^{-1}$ can be assigned to the $\mathrm{C}=\mathrm{O}$ of amide I and carboxylates. The shoulder peak of $1205 \mathrm{~cm}^{-1}$ is due to the $\mathrm{C}-\mathrm{O}$ of polysaccharides and $1148 \mathrm{~cm}^{-1}$ can be assigned to the stretching vibration of hydrogen-bonded $\mathrm{P}=\mathrm{O}$, $\mathrm{O}-\mathrm{C}$ stretching in $\mathrm{P}-\mathrm{O}-\mathrm{C}$ linkage and $\mathrm{P}=\mathrm{OOH}$ groups from phosphates of polyphosphates. The peak of $1071 \mathrm{~cm}^{-1}$ represented the ionized linkage $\mathrm{P}^{+}-\mathrm{O}^{-}$and stretching vibration in P-O-P in acid phosphate esters. The remaining peaks of $970 \mathrm{~cm}^{-1}, 882 \mathrm{~cm}^{-1}$, $780 \mathrm{~cm}^{-1}$ are due to the presence of residual quartz.

Table 3. The summary of related bands in raw FW, soaked FW, FW500, FW600 and FW700 vibration to the functional group or component

| $\begin{aligned} & \text { Wavenumbers } \\ & \left(\mathrm{cm}^{-1}\right) \end{aligned}$ | Vibration | Functional group or component | References |
| :---: | :---: | :---: | :---: |
| 3328-2918 | O-H stretch | Hydroxyl group | [25] |
| 2360-2338 |  | Phosphate compound |  |
| 1706 | $\mathrm{C}=\mathrm{O}$ | Ketones, aldehyde, carboxylic acids and esters | [26], [27], [28] |
| 1650-1612 | $\mathrm{C}=\mathrm{O}$ | Amides I, carboxylates | [26] |
| 1582-1577 | N -H in plane | Amides II | [26] |
| 1386 | O-H bending | Phenol | [27], [29] |
| 1205 | C-O | Polysaccharides | [26] |
| 1190-1130 | $\begin{aligned} & \mathrm{P}=\mathrm{O}, \underset{\mathrm{O}-\mathrm{C}, \mathrm{P}=\mathrm{OOH}}{\text { stretch }} \end{aligned}$ | Phosphate group | [27], [28] |
| 1087-1071 | $\mathrm{P}^{+}-\mathrm{O}^{-}$ | Ionized linkage of acid phosphate esters | $\begin{gathered} {[25] ;[27] ;[28] ;} \\ {[30] ;[31]} \end{gathered}$ |
| 1082 |  | Quartz | [26] |
| 1025-1020 | Si-O stretch | Clay minerals | [26] |
|  | Si-O-Si | Silica |  |
| 982-780 |  | Quartz residual | [32], [33] |

The soaked FW is further carbonized and activated at various activation temperature which the IR spectrum of each temperatures is illustrated in Figure 6. According the figure, it can be observed that the O-H peak at the range of $3197-2918 \mathrm{~cm}^{-1}$ is getting shallower indicating $\mathrm{O}-\mathrm{H}$ group is disappearing as the activation temperature is increasing. The peak observed at $2361 \mathrm{~cm}^{-1}$ attributed to
phosphonates substances in FW500 and further shallower to $2360 \mathrm{~cm}^{-1}$ and $2357 \mathrm{~cm}^{-1}$ in FW600 and FW700 respectively. The peak at $1577 \mathrm{~cm}^{-1}$ in FW500 is assigned to the N-H plane of amides II and further deconvolution resolved the peaks of $1612 \mathrm{~cm}^{-1}$ and $1543 \mathrm{~cm}^{-1}$ which might due to the $\mathrm{C}=\mathrm{O}$ of amides I and N-H plane of amides II as shown in Figure 6(b). The deconvolution of the similar wavenumbers region from $1800-1400 \mathrm{~cm}^{-1}$ is also carried out for FW600 and FW700 as depicted in Figure 6(c, d) which resolved in peaks $1636 \mathrm{~cm}^{-1}$ and $1550 \mathrm{~cm}^{-1}$ in FW600 while $1641 \mathrm{~cm}^{-1}$ and 1540 $\mathrm{cm}^{-1}$ in FW700. This phenomenon showing as the activation temperature, the $\mathrm{C}=\mathrm{O}$ shifted to higher wavenumbers. The stretching $\mathrm{P}=\mathrm{O}$ groups from phosphates of polyphosphates and ionized linkage $\mathrm{P}^{+}$-$\mathrm{O}^{-}$in acid phosphate esters occurring at $1148 \mathrm{~cm}^{-1}$ and $1071 \mathrm{~cm}^{-1}$ in soaked FW are appeared to be at merge into the peak at $1087 \mathrm{~cm}^{-1}$ after activated at $500{ }^{\circ} \mathrm{C}$. This relative peak is then diverted to a doublet at $1130 \mathrm{~cm}^{-1}$ and $1190 \mathrm{~cm}^{-1}$ when activation temperature is increased to $600{ }^{\circ} \mathrm{C}$ and this doublet is remained at almost similar wavenumbers at $700^{\circ} \mathrm{C}$. In FW500 and FW600, the peaks at 979 $\mathrm{cm}^{-1}$ and $982 \mathrm{~cm}^{-1}$ respectively are assigned to quartz residual though this relative peak is shifted to $1020 \mathrm{~cm}^{-1}$ due to clay minerals in FW700. The summary of the related peaks are listed in Table 3.

### 3.2 Electrochemical Performance

CV was carried out over the potential range of -0.9 to -0.3 V , at the scan rate of $1,3,5,7,9,10$, $30,50,70,100 \mathrm{mVs}^{-1}$. Figure 7 (a-c) shows the typical CV of the capacitor. The cells of FW500, FW600 and FW700 exhibit an ideal shape of CV at low scan rate, and have a nearly symmetrical image at about the zero current line for all scan rates, indicating a fast reversible charge/discharge and non-redox behaviour. Additionally, the consistency of the adsorption and desorption of the charge species is preserved, as it shows a symmetrical image at a higher scan rate. In this work, the area under the CV curves enlarges at a higher scan rate, indicating that a higher scan rate promotes higher ion concentration, which significantly influences the formation of the double layer. Consequently, the energy stored increases as the ion migration speed of the electrolyte increases inside the pores of the AC [34]. Figure 8 showing the comparison of CV curve of FW500, FW600 and FW700 at $10 \mathrm{mVs}^{-1}$, it can be seen that the area under the curve is in accordance to the capacitance obtained. The nearly ideal rectangular shape at $100 \mathrm{mVs}^{-1}$ implying the excellent capacitance behavior of the carbon materials and low equivalent series resistance (ESR) [35]. As shown in Figure 9, the capacitance is increasing up to the scan rate of $10-30 \mathrm{mVs}^{-1}$ and depicting a slight drop at further scan rates, however, still maintain at the capacitance higher than the lowest scan rate indicating the stability of electrode material. FW500 has achieved the highest capacitance of $85 \mathrm{Fg}^{-1}\left(10 \mathrm{mVs}^{-1}\right)$ while $65 \mathrm{Fg}^{-1}\left(10 \mathrm{mVs}^{-1}\right)$ and $45 \mathrm{Fg}^{-1}(30$ $\mathrm{mVs}^{-1}$ ) in FW600 and FW700 respectively. The charge-discharge profile is used to determine the electrochemical property and the life cycle of the cell.



Figure 7. Cyclic voltammetry of (a) FW500, (b) FW600 and (c) FW700 in aprotic electrolyte of various scan rates


Figure 8. Comparison of CV curves at $10 \mathrm{mVs}^{-1}$ of FW500, FW600 and FW700


Figure 9. Comparison of capacitance from cyclic voltammetry curve on FW500, FW600 and FW700

In Figure 10(a), the curves showed a nearly symmetrical and triangular shape, which reveals the good capacitive behaviour of the supercapacitor. According to the Figure 7(a), FW500 displayed longest charging and discharging time as compared with FW600 and FW700. The duration of the discharge process, at the $100^{\text {th }}$ and $500^{\text {th }}$ cycles for all carbons, showed an insignificant difference, suggesting that the carbon can withstand high reversibility and stability. The calculated specific capacitance at the $100^{\text {th }}$ and $500^{\text {th }}$ cycles for FW500 ( $107 \mathrm{Fg}^{-1}$ and $105 \mathrm{Fg}^{-1}$ ), FW600 $\left(82 \mathrm{Fg}^{-1}\right.$ and 81 $\mathrm{Fg}^{-1}$ ) and FW700 ( $54 \mathrm{Fg}^{-1}$ and $54 \mathrm{Fg}^{-1}$ ) respectively. The result is in agreement with the specific capacitance evaluated from cyclic voltammetry and showed insignificant difference in capacitance value. The insignificance difference indicated good Coulombic efficiency and capacitive performance of the synthesized carbons in KOH solution [36]. FW500 exhibited high capacitance, owing to its higher surface area and total pore volume, which provide more active site for ions. Additionally, the highest micropore in FW500 provides additional support for ion adsorption enhances the specific capacitance [37]. Particularly, FW500 only showed 8 mV of voltage drop from the start of discharge curve which known as internal resistance (IR). From here, we can see that surface area showed a linear relationship with specific capacitance. Based on Figure 10(b), the results illustrated that all the ACs maintained high stability in capacitance along 500 cycles of charge-discharge.

Nyquist plot, as depicted in Figure 11 showing the imaginary component ( $\mathrm{Z}^{\prime \prime}$ ) of the impedance against the real component ( $Z^{\prime}$ ), indicates the frequency response of the electrode/electrolyte system. All the plots exhibit two different segments which consist of a semicircle loop in the high frequency region and a nearly vertical line in the low frequency region [38]. The observed semicircle loop in the high frequency region indicate the resistance of the electrode/electrolyte/current-collector in the supercapacitor system [39]. The smallest semicircle diameter, depicted in FW600, suggests a lower charge-transfer resistance, which might be attributed to its nearly equivalent ratio of micropore and mesopore volume. However, contradiction was observed between FW500 and FW600, in terms of specific capacitance and charge-transfer resistance.


Figure 10. (a) Charge-discharge curves at 1 mA of FW500, FW600 and FW700 and (b) Specific capacitance of FW500, FW600 and FW700 over 500 cycles

This contradictory result could be the result of less accessible electrolyte into the inner pores, since the total pore volume in the FW600 $\left(0.125 \mathrm{~cm}^{3} \mathrm{~g}^{-1}\right)$ is much lesser, compared to FW500 $(0.248$ $\mathrm{cm}^{3} \mathrm{~g}^{-1}$ ), resulting in lower capacitance.


Figure 11. Nyquist plots for FW500, FW600 and FW700 in electrolytes

## 4. CONCLUSION

A vermicompost-based FW activated carbon was prepared successfully by chemical activation treatment, using $\mathrm{H}_{3} \mathrm{PO}_{4}$. The optimized electrochemical performance of AC was obtained for the FW500 sample. The electrochemical behavior of FW500 in KOH solution showed the specific capacitance of $107 \mathrm{Fg}^{-1}$ and $105 \mathrm{Fg}^{-1}$ at the $100^{\text {th }}$ and $500^{\text {th }}$ cycles respectively while $85 \mathrm{Fg}^{-1}$ obtained from CV curve. The specific capacitance is consistent over 500 cycles. Based on the textural properties, the best capacitance value of FW 500 was found to be controlled by $\mathrm{S}_{\mathrm{BET}}$, total pore volume and pore size distribution. This showed that vermicompost-based AC has potential as a greener electrode material in supercapacitor application.

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