

Numerical Simulation of the Effects of Obstacles in Gas Flow Fields of a Solid Oxide Fuel Cell

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Received: 18 September 2019 / *Accepted:* 23 November 2019 / *Published:* 5 January 2019

In this study, the local transport phenomena and overall cell performance of a single planar anode-supported solid oxide fuel cell with/without rectangular obstacles inside the anode and cathode gas flow channels are numerically investigated by using a three-dimensional mathematical model. Numerical results of two cases including temperature distribution, species concentration distribution, and current density distribution are reported and compared. The results indicate that the maximum temperature of the fuel cell with obstacles is about 5 K lower than that of the fuel cell without obstacles. It is also observed that the hydrogen utilization is improved and a more uniform oxygen distribution is obtained due to the presence of rectangular obstacles. In addition, the pressure drop penalty of the fuel cell with obstacles is greatly increased.

Keywords: Solid Oxide Fuel Cells, Numerical modeling, Gas flow channel geometry, Obstacles

1. INTRODUCTION

Solid oxide fuel cells (SOFCs) are one of the promising technologies for future energy conversion demands due to their high efficiency and the clean energy. The components of SOFCs stack include: anode electrode, electrolyte, cathode electrode and interconnect. The fundamental mechanism of a SOFC includes the oxidation of fuel at anode electrode and the reduction of oxygen at cathode electrode. Due to the high electrical performance, many researches have focused on the structures, materials, and operating conditions of SOFCs [1-6]. Over the past decades, many researchers focused on the structural optimization of SOFCs. Investigations related to the design of gas channels and interconnectors have been reported [7-12].

The local transport characteristics and overall cell performance is significantly affected by the flow field design. The heat and mass transport characteristics in fuel cell ducts with rectangular and trapezoidal cross-section were numerically investigated [13]. Numerical studies were performed to investigate the effect of geometric parameters on the flow uniformity in planar SOFC stacks [14]. An innovative shape was adopted to improve the cell performance [15]. Nickel foam and metallic corrugated structure were used as gas distributor and current collector in the anode and cathode sides of SOFCs, respectively [16]. Recently, the gas transport process and cell performance were significantly improved when finger-like channels were employed in SOFCs [17]. The cell performance of SOFCs with woven meshes as the anode flow field was experimentally investigated and reported [18]. The cell performance of SOFCs with six different flow field designs was numerically studied and compared [19].

Understanding the detailed transport phenomena occurring within SOFCs is an expensive and challenging procedure. Therefore, numerical simulation plays an important role in predicting the local transport processes and overall performance of SOFCs. An appropriate design of flow field channel is beneficial to the reactant gas transport as well as the cell performance. In this present study, the cell performance of a planar anode-supported SOFC with rectangular obstacles inside the anode and cathode gas channels have been investigated and compared with that with straight gas flow channels.

In the three-dimensional mathematical model, the mass, momentum, species, energy and charge conservation equations are simultaneously solved. With the simulation results, the local temperature distributions and the species concentration distributions of the fuel cells with/without obstacles are presented and discussed. In addition, the current density distributions and pressure drop are also presented.

2. MODEL AND NUMERICAL METHOD

2.1 Model geometry

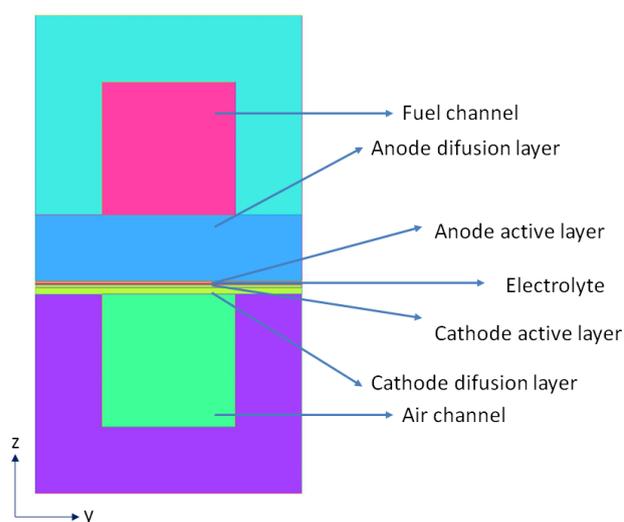


Figure 1. Schematic of a SOFC.

Schematic illustration of the proposed fuel cell physical model can be seen in Figure 1 and Figure 2. In the anode and cathode gas flow channels, five rectangular obstacles are located in the middle of the channel. The geometric parameters of the model are summarized in Table 1.

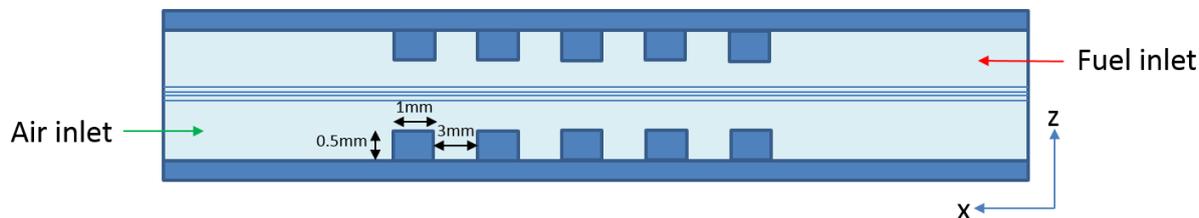


Figure 2. The SOFC with obstacles inside gas flow channels.

Table 1. Fuel cell geometry parameters

Parameters	Value	Units
Cell length	40	mm
Cell width	2	mm
Channel width	1	mm
Channel height	1	mm
Anode diffusion layer thickness	0.5	mm
Anode active layer thickness	0.02	mm
Cathode active layer thickness	0.02	mm
Cathode diffusion layer thickness	0.05	mm
Electrolyte thickness	0.01	mm
Interconnect height	1.5	mm
Obstacle height	0.5	mm
Obstacle length	1	mm

Table 2. Properties for different components

Properties	Value
Anode porosity $[\epsilon]$	0.5
Cathode porosity $[\epsilon]$	0.5
Anode conductivity σ $[1/(\text{ohm}\cdot\text{m})]$	100000
Cathode conductivity σ $[1/(\text{ohm}\cdot\text{m})]$	7700
Permeability β $[\text{m}^2]$	1.0×10^{-12}
Anode active surface area to volume ratio A_{an} $[1/\text{m}]$	200000
Cathode active surface area to volume ratio A_{cat} $[1/\text{m}]$	200000
Anode exchange current density $i_{an,ref}$ $[\text{A}/\text{m}^2]$	5300
Cathode exchange current density $i_{cat,ref}$ $[\text{A}/\text{m}^2]$	2000
Thermal conductivity of diffusion layer k $[\text{W}/(\text{m}\cdot\text{K})]$	11
Thermal conductivity of catalyst layer k $[\text{W}/(\text{m}\cdot\text{K})]$	6
Thermal conductivity of electrolyte k $[\text{W}/(\text{m}\cdot\text{K})]$	2.7
Thermal conductivity of interconnect k $[\text{W}/(\text{m}\cdot\text{K})]$	6

The parameters used in the mathematical model are summarized in Table 2. The mesh density in different zones is varied to ensure the accuracy of computations, as shown in Fig.3.

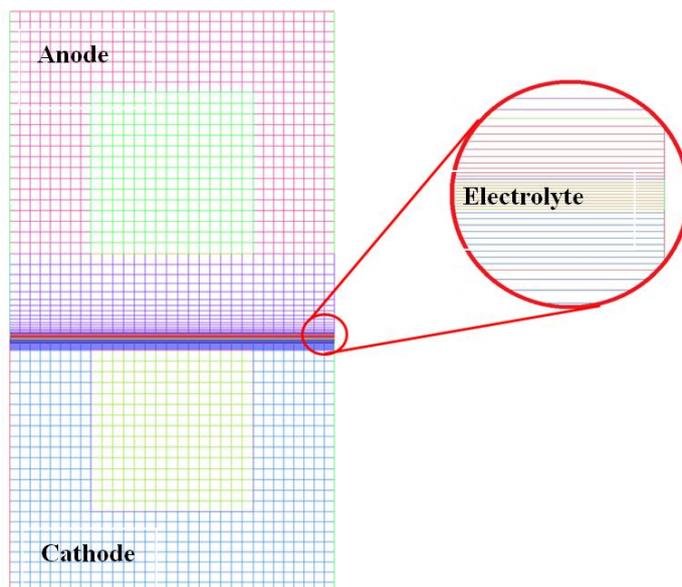


Figure 3. Mesh of the computational domain.

2.2 Model assumptions

The assumptions used in this study are as follows:

- (1) The fuel cell is under steady state.
- (2) The fluid flow in the gas channels is laminar flow.
- (3) The ideal gas law is applied for reactant gases.
- (4) The diffusion and active layers are homogeneous and isotropic.

2.3 Governing equations

In the three-dimensional mathematical model, the conservation equations of mass, momentum species, momentum, energy and charge were solved using the finite-volume method. The solid and fluid domains were divided into discrete meshes, and the equations are specified for various zones in the full cell.

The continuity conservation equation:

$$\nabla(\rho U) = S_m \quad (1)$$

where ρ is the mixture density. S_m , source term is expressed as:

$$S_m = \begin{cases} \sum_i S_{m,i} & \text{active layers} \\ 0 & \text{others} \end{cases}$$

The momentum conservation equation:

$$\nabla(\rho UU) = -\nabla P + \nabla(\mu \nabla U) + S_d \quad (2)$$

where U is the velocity vector, P is the pressure and μ is the dynamic viscosity. S_a , source term is described as:

$$S_a = \begin{cases} 0 & \text{others} \\ -\frac{\mu}{\beta} U & \text{active and diffusion layers} \end{cases}$$

where β is the permeability of the porous structure.

The species conservation equation:

$$\nabla(\rho U Y_i) = \nabla(\rho D \nabla Y_i) + S_{m,i} \quad (3)$$

where Y_i is the mole fraction of the i th species, D is the mass diffusion coefficient and $S_{m,i}$ is the source term resulting from chemical reactions. The Stefan-Maxwell equation is used to calculate the gas species mass diffusivity.

$S_{m,i}$, source terms is expressed as:

$$S_{m,i} = \begin{cases} \frac{j}{n_e F} M_i & \text{active layers} \\ 0 & \text{others} \end{cases}$$

where M_i is the molecular weight of the i th species and J is the current density.

The energy conservation equation:

$$\nabla(\rho C_p U T) = \nabla(k_{eff} \nabla T) + S_T \quad (4)$$

where k_{eff} is the effective thermal conductivity of the solid and gas phases. S_T , source term accounts the ohmic heating, activation losses, the reversible heat due to electrochemical reactions and the heat of chemical reactions. Ohmic heating takes place in the electrolyte and electrodes while the other heat source terms are located in the active layers.

$$k_{eff} = (1 - \varepsilon)k_s + \varepsilon k_f$$

$$S_T = \begin{cases} \frac{j^2}{\sigma} + j \cdot \eta_{act} + \frac{j}{n_e} T \Delta S & \text{active layers} \\ 0 & \text{others} \end{cases}$$

where η_{act} is the activation potential, ΔS is the entropy change associated with the electrochemical reactions, and σ is the electrical conductivity.

The charge conservation equation:

$$\nabla(\sigma_{sol} \nabla \phi_{sol}) + S_s = 0 \quad (5)$$

$$\nabla(\sigma_{ionic} \nabla \phi_{ionic}) + S_{ionic} = 0 \quad (6)$$

Where σ is electrical conductivity, ϕ is electric potential, and S is the source term.

$$\sigma_{ionic} = \frac{100}{0.3685 + 0.002838e^{(10300/T)}}$$

$$S_s = \begin{cases} -j_a & \text{anode active layer} \\ j_c & \text{cathode active layer} \end{cases}$$

$$S_{ionic} = \begin{cases} j_a & \text{anode active layer} \\ -j_c & \text{cathode active layer} \end{cases}$$

The source term S_s and S_{ionic} are described by the Butler-Volmer functions:

$$j_a = i_{an.ref} A_{an} \left(\frac{C_{H_2}}{C_{H_2.ref}} \right)^{\frac{1}{2}} \left(e^{\frac{\alpha_a F \eta_a}{RT}} - e^{-\frac{-\alpha_c F \eta_a}{RT}} \right)$$

$$j_c = i_{cat.ref} A_{cat} \left(\frac{C_{O_2}}{C_{O_2.ref}} \right) \left(e^{-\frac{-\alpha_c F \eta_c}{RT}} - e^{\frac{\alpha_a F \eta_c}{RT}} \right)$$

$$\eta_a = \phi_{sol} - \phi_{ionic}$$

$$\eta_c = \phi_{sol} - \phi_{ionic} - V_{oc}$$

2.4. Boundary conditions and solution methods

The computational domain consists of a single cell which operates in counter-flow, i.e., the fuel flow direction is opposite to the oxygen flow direction. A three-dimensional model is implemented using the commercial software ANSYS FLUENT with its fuel cell add-on module. The input parameters and boundary conditions for the two geometries depicted in Fig.1 are shown in Table3.

Table 3. Parameters used in simulation

Title	Value
Anode mass flow rate	2×10^{-8} kg/s
Anode inlet temperature	1073 K
Anode fluid composition	$Y_{H_2}=0.95$; $Y_{H_2O}=0.05$
Cathode mass flow rate	8×10^{-7} kg/s
Cathode inlet temperature	1073 K
Cathode fluid composition	$Y_{O_2}=0.21$; $Y_{N_2}=0.79$
Operating pressure	1 atm
Operating voltage	0.7 V
Open circuit voltage	1.1 V

At the inlet of anode and cathode gas flow channels, the mass flow rate, temperature and species composition are specified. While the pressure boundary condition is specified at the outlet of the flow channel. The gas flow channel surfaces facing current collectors are specified as “wall” boundary condition. All other external boundaries are the solid wall. The electronic potential at the anode current collector is set to 0 and the electronic potential at the cathode current collector is set to the cell operating voltage (0.7 V in this study). The Semi-Implicit Method for Pressure Linked Equations (SIMPLE) algorithm is used to solve pressure-velocity coupling. The second-order discretization scheme is employed to the convection terms of all equations except for pressure where the standard scheme is used. When the continuity residual for all equations was less than 10^{-6} , the solution is considered as converged. Three mesh systems (400,000, 650,000 and 900,000 elements) are used to test the mesh independence at operating voltage 0.7 V. And the second mesh system was chosen for the following computations in order to balance the accuracy and computational resources.

3. SIMULATION RESULTS AND DISCUSSION

3.1 Temperature distribution

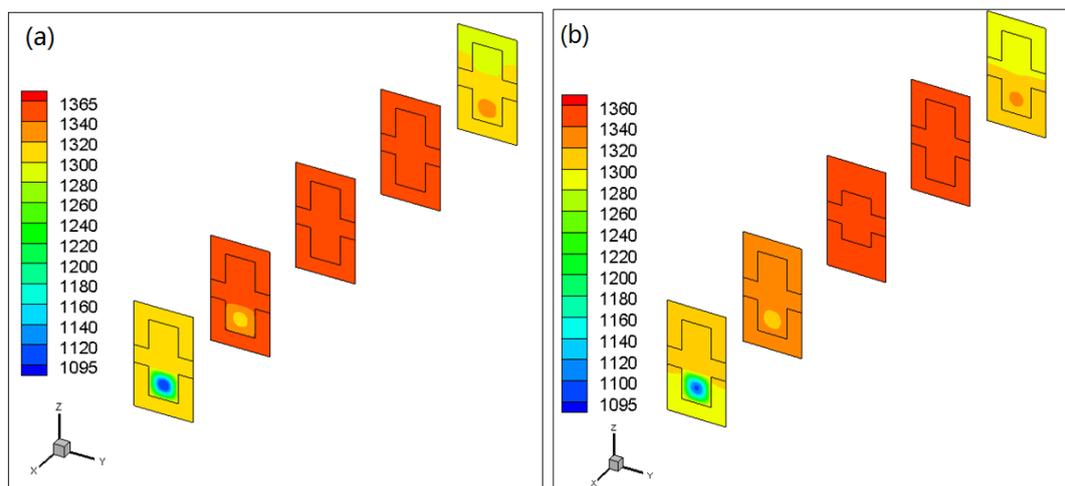


Figure 4. Temperature distribution at different positions along gas flow direction ($x=0.001\text{m}$, 0.01m , 0.02m , 0.03m , 0.039m): (a) straight channel; (b) channel with obstacles.

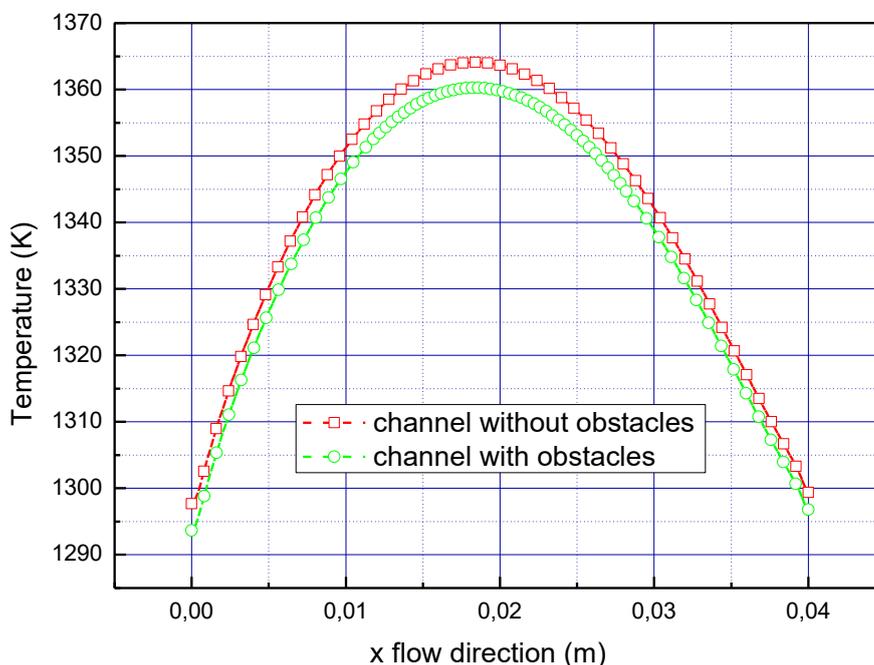


Figure 5. Comparison of temperature distribution along the middle line of the active area of two different channels.

Figure 4 depicts the temperature distribution of straight channel and channel with obstacles at different position along gas flow direction ($x=0.001\text{m}$, 0.01m , 0.02m , 0.03m , 0.039m), respectively. Figure 5 compares the temperature distribution along the middle line of the active area of the two different channel geometries. It is clear that the maximum temperature occurs around the middle region of the channel due to the counter flow arrangement in this study. This is consistent with the results reported in the numerical study [20-21]. The temperature distribution is significantly affected by the

flow arrangements (co-flow, counter-flow, and cross-flow) [20]. It is also observed that the maximum temperature obtained in the fuel cell with obstacles is about 5 K lower than that without obstacles. It is indicated that the temperature gradient is decreased due to the presence of obstacles in the flow channels. When the temperature gradient is too high, it is harmful to the performance and lifetime of the SOFCs. Therefore, the application of obstacles in the gas flow channels has a potential ability to obtain a more uniform temperature distribution in the fuel cell.

3.2. Mass transport characteristics

3.2.1 Hydrogen distribution

As shown in Figure 6, the mole fraction distribution of hydrogen is presented for both fuel cells with/without obstacles.

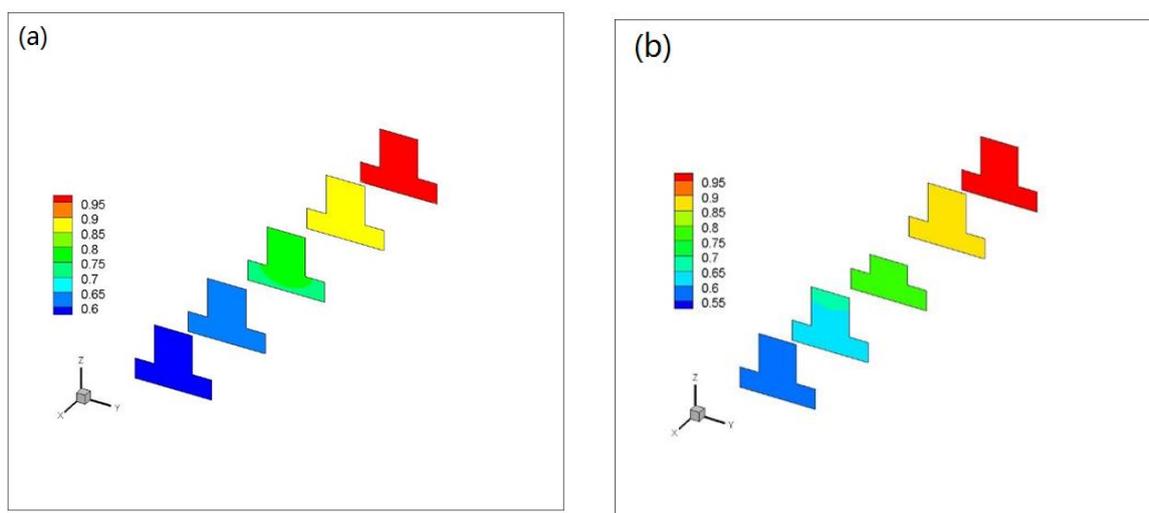


Figure 6. Hydrogen mole fraction in the anode side at different positions along gas flow direction ($x=0.001\text{m}$, 0.01m , 0.02m , 0.03m , 0.039m): (a) straight channel; (b) channel with obstacles.

With the consumption of hydrogen and generation of water caused by the electrochemical reaction, the mole fraction of hydrogen decreases from the inlet to the outlet. As can be seen in Figure 6, the mole fractions of hydrogen at the inlet and outlet are 0.95 and 0.6, respectively. Thus, the fuel utilization of the fuel cell without obstacles is about 0.37. Compared with the fuel cell without obstacles, the fuel cell with obstacles has a smaller mole fraction at the flow channel outlet which is about 0.55. The fuel utilization of the fuel cell with obstacles is about 0.42. The application of obstacles in gas flow channels increases the hydrogen utilization, which is expected for the fuel cell.

3.2.2 Oxygen distribution

Figure 7 illustrates oxygen mole fraction distribution throughout the cathode side of the full cell with/without obstacles at the cell voltage of 0.7 V. Figure 8 compares the oxygen mole fraction

distribution in the cathode along the middle line of the active area of two different channels. It can be seen that oxygen mole fraction decreases along the flow direction for both cases due to the consumption of the oxygen, which is needed for the electrochemical reaction. In addition, the oxygen mole fraction of the fuel cell with obstacles is higher than that of fuel cell without obstacles, especially at the regions where the obstacles are placed. It is also observed that the oxygen mole fraction is higher at the regions under the channels than that at the regions under the ribs. That is because the oxygen diffusion to the regions under the ribs is limited by the diffusion lengths. The variation of oxygen distribution along the flow direction is obtained due to the existence of obstacles in the gas flow channel. The similar behavior was also observed in the fuel cells with wavy surface cathode gas flow channel [22].

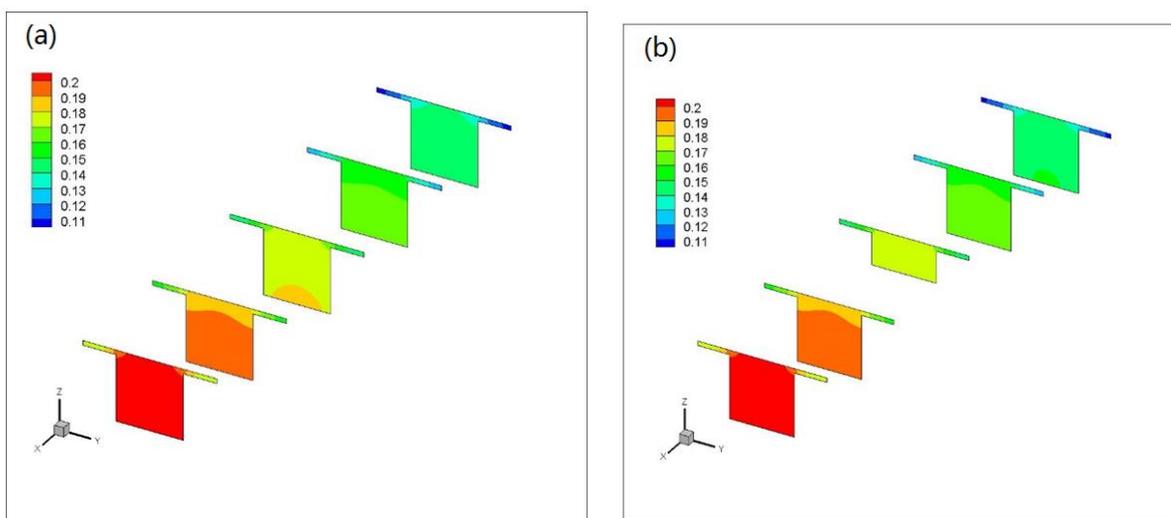


Figure 7. Oxygen mole fraction in the cathode side at different positions along gas flow direction ($x=0.001\text{m}, 0.01\text{m}, 0.02\text{m}, 0.03\text{m}, 0.039\text{m}$): (a) straight channel; (b) channel with obstacles.

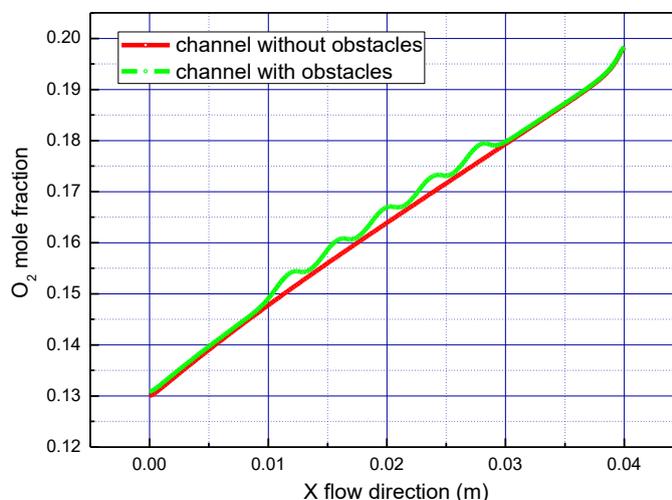


Figure 8. Oxygen mole fraction distribution in the cathode along the middle line of the active area of two different channels.

3.3. Current density distribution

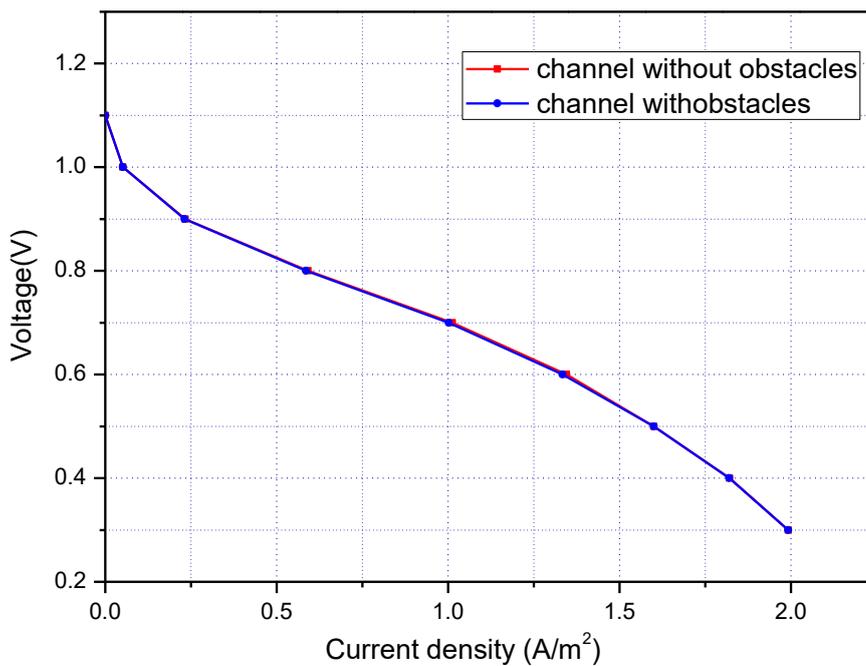


Figure 9. Comparison of polarization curves between the two different fuel cells.

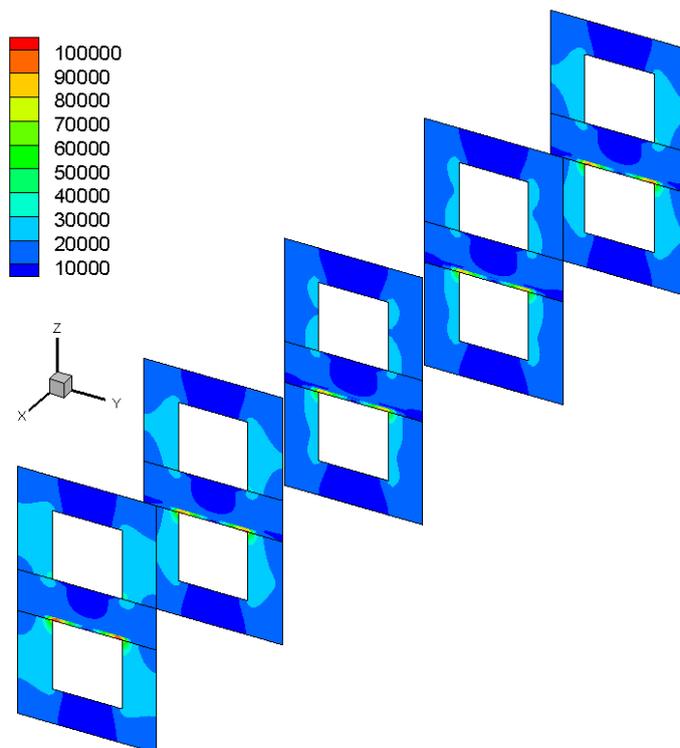


Figure 10. Current density distribution at different positions along the main flow direction for the fuel cell without obstacles.

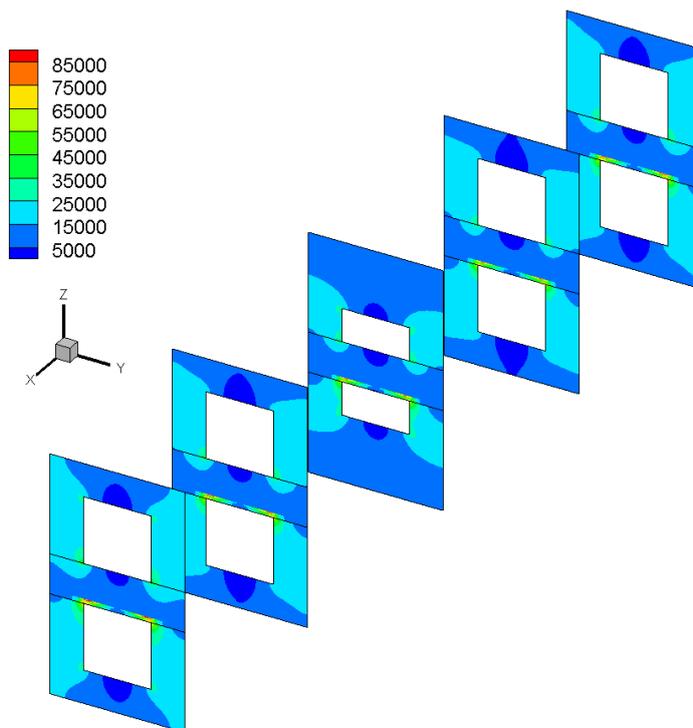


Figure 11. Current density distribution at different positions along the main flow direction for the fuel cell with obstacles. the

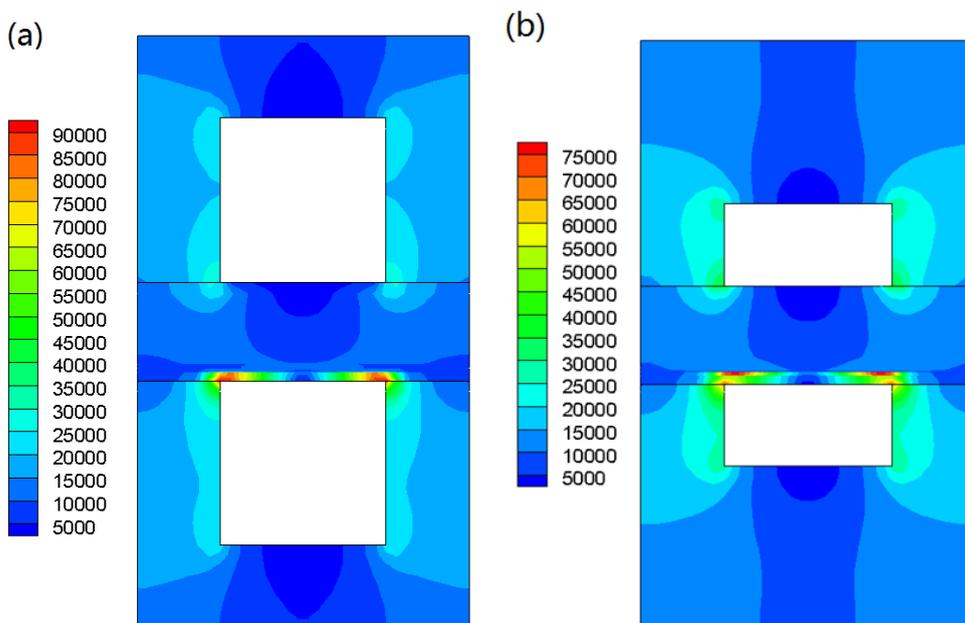


Figure 12. Current density distribution in $x=0.2$ m along the main flow direction: (a) straight channel; (b) channel with obstacles.

Comparison of polarization curves between the two different gas flow channels are shown in Figure 9. The effects of the obstacles on the overall cell performance are very small compared with straight channel. Similarly, the cell performance of SOFCs with co-flow and counter flow is almost the same. However, the local transport processes are different for two cases [20]. The cell performance can

be affected by the position, size, number and shape of the obstacles in the gas flow channels, which should be further studied. Figure 10 and 11 depict the current density distribution in different positions along the main flow direction for the two different cases.

In Figures 10 and 11, it can be seen that the current density distribution is uneven for both two channel geometry fuel cell. It is shown that the highest current density appears in the cathode side at the corners between ribs and electrode. At the anode side, it is also has the same trend, but the maximum value is much smaller than the cathode side which is due to the relative thick anode layer.

Figure 12 compares the current density distribution in the middle of the channel ($x=0.2$ m) along the main flow direction for the two full cells. It is found that the maximum current density of fuel cell without obstacles is larger than that of fuel cell with obstacles, which is mainly attributed to the temperature distribution and the presence of obstacle. The electron transport resistance is increased due to the increase in interconnect thickness. A higher current density results in a higher over potential and a higher ohmic heat generation in fuel cells. Both the uneven and higher current density are harmful to the fuel cell performance and lifetime.

3.4. Pressure drop

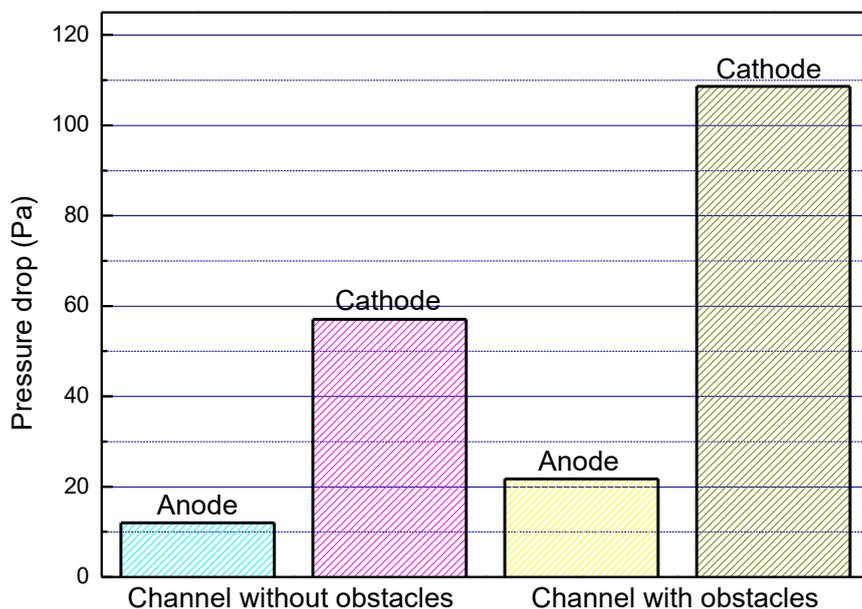


Figure 13. Pressure drop in anode and cathode of the two different fuel cells.

Figure 13 shows the pressure drop in the anode and cathode gas flow channels for two cases. For both cases, the pressure drop in cathode side is higher than the anode side. For the fuel cell with obstacles, the cathode pressure drop and anode pressure drop is 109 Pa and 21 Pa, respectively. And for the fuel cell without obstacles, the cathode pressure drop and anode pressure drop is 58 Pa and 12 Pa, respectively.

It also can be seen that with the obstacles inside the gas flow channel, the pressure drop increased almost by one time compared with the channel without obstacles. It is obvious that the pressure drop is greatly increased when the obstacles are adopted in the gas flow channel. The similar results were also reported in the previous literature [22]. In addition, the pressure drop is significantly affected by the cross-sectional shape [13, 15, 23] and flow field design [16, 17, 19, 24].

4. CONCLUSIONS

A three-dimensional mathematical model has been employed to investigate the performance of fuel cells with/without obstacles in the gas flow channels. Simulation results including distributions of temperature, species concentration and current density inside fuel cells are presented. The results indicate that the maximum temperature of the fuel cell with obstacles is about 5 K lower than that of the fuel cell without obstacles. The application of obstacles in gas flow channels increases the hydrogen utilization which is expected for the fuel cell. The maximum current density appears in the cathode side at the corners between ribs and electrode. The average current density is almost the same for both cases. However, the local current density is significantly affected by the presence of obstacles. The effects of position, size, number and shape of the obstacles in the gas flow channels can be further studied.

NOMENCLATURE:

A	Specific active surface area, 1/m
C_P	Specific heat, J/(kg·K)
D	Diffusion coefficient, m ² /s
F	Faraday constant, 96487 C/mol
i	Exchange current density, A/m ²
j	Transfer current density, A/m ³
k	Thermal conductivity, W/(m·K)
M	Molecular weight, kg/mole
n_e	Number of electrons transferred per reaction
P	Pressure, Pa
R	Universal gas constant, 8314J/(mol·K)
S	Entropy, kJ mol ⁻¹ K ⁻¹
S	Source term
T	Temperature, K
U	Velocity vector, m/s
V	Voltage, V
Y_i	Mole fraction of species i

Greek Symbols

β	Permeability, m ²
ε	Porosity
η	Overpotential, V
μ	Dynamic viscosity, kg/(m·s)

ρ	Density, kg/m ³
σ	Electrical conductivity, 1/ohm m
Φ	Electric potential, V

Subscripts

<i>an</i>	Anode
<i>cat</i>	Cathode
<i>eff</i>	Effective
<i>i</i>	Gas species <i>i</i>
<i>m</i>	Momentum
<i>oc</i>	Open circuit
<i>ohm</i>	Ohmic

ACKNOWLEDGEMENT

The authors acknowledge the financial supports of the National Natural Science Foundation of China (No.51606013).

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