Effects of Al Content on the Corrosion Behaviors of Low Cr Bearing Steels in NaCl Solutions

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The effects of Al content on the corrosion behaviors of aluminum-bearing steels were studied in NaCl solutions. Electrochemical measurements and Raman and scanning electron microscopy (SEM) surface analyses revealed that the aluminum-bearing steel formed two passivation films: the outer layer film contained Al₂O₃ and Cr₂O₃, and the inner layer film contained lepidocrocite (γ-FeOOH), regardless of whether the NaCl solution was faintly acidic/alkali or neutral. Lepidocrocite is unstable and can transform to α-Fe₂O₃ and γ-Fe₂O₃ when exposed to air. The electrochemical impedance spectroscopy (EIS) results showed that the dominant anticorrosion effect comes from the inner layer film, but a larger Al content causes a larger charge transform resistance and larger outer and inner passive resistances, which result in better anticorrosion properties. Furthermore, corrosion weight gain tests revealed that the Al content (Al%) and corrosion rate (V) exhibit a negative linear relationship V = -1.3667Al % (wt.%) +1.9691 in the investigated conditions.

Keywords: Bearing steel; Al; Corrosion weight gain; Polarization curve; EIS; Raman spectra.

1. INTRODUCTION

Bearing steels are widely used in the aviation, spaceflight and project equipment fields [1]. With the rapid growth of modern science and technology and the wide application of bearing steels, society has put forward new requirements and higher expectations for the performances of bearing steels. For example, in the spacecraft and deep-sea exploration fields, bearing steels must exhibit reliable temperature resistant, antimagnetic and anticorrosion performances, and some metal elements must be
added to bearing steels (such as Cr and Cu) to fill some defects in the original bearing steel, which improves or changes some properties to meet the actual needs of the material [2-4]. Yamashita et al. [5] investigated the structures of protective rust layers, which formed on weathering steels by long-term exposure in industrial atmospheres in Japan and North America. They noted that the innermost Cr-substituted goethite layer may be the final modus of the protective rust layer, which can inhibit the penetration of corrosive substances through the rust layer, thereby slowing down further corrosion. In a CO₂ solution system, bearing steel with added Cr not only had a smaller general corrosion rate but also had smaller local corrosion [6]. By adding Cr and Al, Tsai et al. [7] achieved Ti-Cr-bearing hot-rolled dual-phase steel with a superior combination of mechanical properties. Due to the considerable strengthening obtained from interphase-precipitated nanometer-sized carbides in ferrite, this dual-phase steel has a yield ratio of approximately 0.72, which is much higher than those of conventional dual-phase steels. Copper is also often added to steel. Wang et al. [8] studied Cu-bearing stainless steel scaffolds with two different structures (body centered cubic and gyroid labyrinth) at two solid fractions (25% and 40%). The results revealed that Cu has the potential to lessen implant-associated infections. Compared to the 316L scaffold, the addition of Cu to the bearing stainless steel did not significantly affect the strength and stiffness; these results coupled with the addition of antimicrobial Cu may supply a new orientation for medical stainless steels.

Al is a good deoxidizing agent in the aluminum-bearing steel industry that has a good anti-fatigue property. Twenty years ago, people added Al to bearing steel and produced fine grain sizes and thus reduced the hardenability of steel [9]. Since then, many studies have been carried out to probe the effects of different aluminum contents on the fatigue properties, deformation and precipitation behavior, and mechanical properties of bearing steel. Yang et al. [10] investigated the effects of aluminum content on fatigue properties and the corresponding crack initiation and propagation behavior of bearing steel in a very high cycle fatigue regime. The results showed that in the highly clean GCr15 bearing steel, high Al content tends to form a collection area of Al₂O₃ particles; therefore, bearing steel with high Al content has poor fatigue properties due to the large size of the crack initiation region. In contrast, bearing steel with low Al content possesses relatively better fatigue properties because single complicated oxides mainly containing Al₂O₃ are smaller. Wang et al. [11] investigated the effects of deformation amount, deformation temperature and subsequent holding time on the deformation spheroidizing process of high-carbon-bearing steel containing aluminum. The experiment display that the spheroidization period can be shortened by the deformation spheroidizing treat. High deformation temperatures and deformation amounts cause the coarsening of carbides. However, at a lower deformation temperature, the amount of deformation will slightly affect the diameter and roundness of the carbide. When the aluminum content is less than 0.75%, the addition of aluminum inhibits the growth of carbides and ameliorates their roundness. Yang et al. [12] studied the influence of Al alloy on the hot deformation behavior of bearing steel. The results indicate that the addition of Al significantly increases the flow stress of steel due to the strong strengthening effect of Al on the austenite phase, and accelerates the strain softening rates due to the effect of the increasing stacking fault energy, which indicates that Al alloying reduces the high-temperature plasticity and the positive effect of Al on bearing steel. To define the role of aluminum in the precipitation behaviors and mechanical properties of Cu-Ni-bearing low alloy steels, Liu et al. [13] studied their microstructures and precipitation behaviors via electron microscopy combined with
thermodynamic analyses. Aluminum had a great effect on the precipitation behavior of niobium, wherein the precipitation temperature of Nb(C, N) was decreased and the prior austenite grain size was controlled by the Al and Nb precipitation. In addition, aluminum effectively increased the precipitate density by increasing the ordered-B2 Ni(Al, Mn) nucleation rate and copper precipitation.

Another important parameter to evaluate the performance of aluminum-bearing steel is its anticorrosion character. Miki [14] studied the corrosion behaviors of aluminum-bearing steels in strongly concentrated nitric acid solutions. The results displayed that the addition of aluminum to stainless steel resulted in the inhibition of corrosion for stainless steels in the liquid phase, but no inhibition effect was observed in the vapor phase. Nishimura [15] compared the corrosion electrochemical behaviors of Si- and Al-bearing steel and carbon steel. The results revealed that, compared with the carbon steel, the Si- and Al-bearing steel exhibited outstanding corrosion resistance in the exposure test. The causes were that Si and Al mainly existed in nanoscale iron composite oxides in the internal rust formed by the steel, which makes the steel containing Si and Al have higher rust resistance and corrosion resistance reactivity compared to those of carbon steel. In summary, previous studies on aluminum-bearing steel corrosion behaviors were relatively lacking. Hence, in this work, different contents of aluminum were added to bearing steels, and then the corrosion behaviors of aluminum-bearing steel specimens were studied via electrochemical techniques and surface analyses for the following reasons: (1) investigate the electrochemical mechanism of aluminum-bearing steel in different pH NaCl solutions and (2) understand the effects of aluminum content on aluminum-bearing steel corrosion behaviors and provide experimental proof for the corrosion assessment of Al-bearing steel in environments with different acidities/basicities (pH 5.0-9.0).

2. EXPERIMENT

2.1 Aluminum-bearing steel production and electrode preparation

Three GCr15SiAlMo bainitic bearing steel specimens were used in this study. These three specimens were made from GCr15SiMo steel, and their smelting process was double vacuum smelting (vacuum induction + vacuum consumption) [12], which provide a lower purity oxygen and higher purity and lower oxide inclusions, which increase the material contact fatigue life [16]. The three aluminum-bearing steel specimens were labeled as 100D, 100E and 100F, and the elemental analyses for these samples are shown in Table 1.

Table 1. EDS elemental analysis of the Aluminium-bearing steel samples (Wt.%)

<table>
<thead>
<tr>
<th>Bearing steel number</th>
<th>C</th>
<th>Mn</th>
<th>Si</th>
<th>Cr</th>
<th>Mo</th>
<th>Al</th>
<th>P</th>
<th>S</th>
</tr>
</thead>
<tbody>
<tr>
<td>100D</td>
<td>0.998</td>
<td>0.260</td>
<td>0.740</td>
<td>1.540</td>
<td>0.330</td>
<td>0.430</td>
<td>0.004</td>
<td>0.002</td>
</tr>
<tr>
<td>100E</td>
<td>1.020</td>
<td>0.230</td>
<td>0.700</td>
<td>1.510</td>
<td>0.340</td>
<td>0.750</td>
<td>0.005</td>
<td>0.002</td>
</tr>
<tr>
<td>100F</td>
<td>0.993</td>
<td>0.240</td>
<td>0.830</td>
<td>1.540</td>
<td>0.350</td>
<td>0.970</td>
<td>0.004</td>
<td>0.002</td>
</tr>
</tbody>
</table>
The steel specimens were cut into cuboid shapes \((1.0 \times 1.0 \times 0.3 \text{ cm})\) to ensure their bottom surfaces, the working area, was \(1.0 \text{ cm}^2\). Then, connect the specimen to the copper wire by using silver paint on the upper surface, and then the specimens were sealed with epoxy resin to ensure that only the working surface was exposed to the solution.

2.2 Corrosion weight gain test

In this work, the corrosion weight gain method was adopted [17]. The three GCr15SiAlMo bearing steels specimens were cut into cuboid samples with \(1.0 \times 1.0 \times 0.3 \text{ cm}\) dimensions, and each kind of steel specimen, 100D, 100E and 100F, had 3 pieces. Prior to the hanging piece corrosion gain test, the steel specimens were polished with a sequence of 1.0, 0.3, and 0.05 \(\mu\text{m}\) alumina powder to obtain a fresh surface, and then the specimens were degreased using alcohol, rinsed with deionized water and dried in a stream of air. The exact dimensions of the 9 steel specimens were measured with Vernier calipers and their exact weights before \((W_0)\) and after \((W_1)\) corrosion were recorded with an electronic balance. Then, the 9 steel specimens were soaked in 9 bottles containing 3.5\% (wt. \%) NaCl solution that adopted the hanging piece method; after 20 days of corrosion, the specimens were removed and weighed. The obtained data were employed to calculate the corrosion rate \(V\) (mm/a) according to Eq. (1), which indicates either a decrease or increase in the thickness of a metal surface due to corrosion within one year.

\[
V=8.76 \times 10^4 \times \frac{W_1-W_0}{STD}
\]

(1)

Where \(W_1\) is the weight of the steel specimen after corrosion (g); \(W_0\) is the initial weight of the steel specimen (g); \(S\) is the surface area that was soaked in the NaCl solution (cm\(^2\)); \(T\) is the corrosion time (h) and \(D\) is the density of the steel specimen (g/cm\(^3\)).

2.3 Electrochemical measurements

Electrochemical measurements were performed with an electrochemical measurement system (PARSTAT 2273, Princeton Applied Research) controlled by a personal computer. In this work, a traditional three-electrode electrolytic cell system was used, in which platinum was used as the auxiliary electrode, bearing steel was used as the working electrode, and the reference electrode was a saturated calomel electrode (SCE). Unless otherwise stated, the standard hydrogen electrode (SHE) was cited for all other potentials. The reference electrode was connected to a Luggin capillary, so that the solution resistance between the working electrode and the reference electrode can be minimized. HCl and NaOH solutions were used to adjust the pH of the 3.5\% (wt. \%) NaCl electrolyte solutions to 5.0, 7.0 and 9.0. Analytical grade reagents were used in the experimental investigation.

The polarization curves started a potential from -600 mV and ended at +600 (vs. open current potential, OCP). During the measurement, the scan rate was 1.0 mV·s\(^{-1}\). The EIS tests were obtained at open current potential in the frequency range of 1 mHZ-10 KHz with amplitude of 10 mV. Then, using
the ZSimpWin 3.20 (2004) software to fit the impedance data. The experiments were conducted at 25 ± 1°C.

2.4 Scanning electron microscopy (SEM) and Raman spectral analysis

Three 10 mm × 10 mm × 3 mm steel samples were used for the surface analyses. Three steel samples were immersed in a 36.28 g/L NaCl solution. After 15 days of corrosion, SEM (SU5000, Hitachi of Japan) was used to observe the corrosion morphologies of the specimens, and Raman spectral analyses (British Renishaw) were used to analyze the surface characteristics of the specimens at a wavelength of 514 nm during the test. The collection time was 10 s.

3. RESULTS AND DISCUSSION

3.1 Corrosion weight gain test study

Table 2. Corrosion weight gain test results of the Aluminium-bearing steel samples

<table>
<thead>
<tr>
<th>Sample</th>
<th>Size (mm<em>mm</em>mm)</th>
<th>W₀ (g)</th>
<th>W₁ (g)</th>
<th>Corrosion rate (mm/a)</th>
<th>Average corrosion rate (mm/a)</th>
</tr>
</thead>
<tbody>
<tr>
<td>100D-1</td>
<td>10.18<em>9.32</em>2.41</td>
<td>1.8852</td>
<td>2.0850</td>
<td>1.5586</td>
<td>1.3887</td>
</tr>
<tr>
<td>100D-2</td>
<td>10.28<em>9.32</em>2.41</td>
<td>1.9038</td>
<td>2.0953</td>
<td>1.4816</td>
<td></td>
</tr>
<tr>
<td>100D-3</td>
<td>10.28<em>9.32</em>2.52</td>
<td>1.9906</td>
<td>2.1383</td>
<td>1.1258</td>
<td></td>
</tr>
<tr>
<td>100E-1</td>
<td>9.44<em>9.20</em>2.38</td>
<td>1.9267</td>
<td>2.0209</td>
<td>0.7940</td>
<td>0.9261</td>
</tr>
<tr>
<td>100E-2</td>
<td>9.75<em>9.62</em>2.55</td>
<td>1.9660</td>
<td>2.0992</td>
<td>1.0289</td>
<td></td>
</tr>
<tr>
<td>100E-3</td>
<td>9.62<em>9.59</em>2.55</td>
<td>1.9481</td>
<td>2.0701</td>
<td>0.9553</td>
<td></td>
</tr>
<tr>
<td>100F-1</td>
<td>9.58<em>9.26</em>2.55</td>
<td>1.8782</td>
<td>1.9724</td>
<td>0.7555</td>
<td>0.6540</td>
</tr>
<tr>
<td>100F-2</td>
<td>9.42<em>9.24</em>2.54</td>
<td>1.8500</td>
<td>1.9146</td>
<td>0.5270</td>
<td></td>
</tr>
<tr>
<td>100F-3</td>
<td>9.62<em>9.71</em>2.80</td>
<td>2.1678</td>
<td>2.2592</td>
<td>0.6795</td>
<td></td>
</tr>
</tbody>
</table>

Table 2 shows the corrosion weight gain results of the three aluminum-bearing steel specimens. From the table, we can see that the aluminum-bearing steel corrosion rates were 1.3887, 0.9261 and 0.540 mm/a when the Al contents were 0.430, 0.750 and 0.970 (wt. %), respectively. The results showed that as the Al content increased, the aluminum-bearing steel corrosion rate decreased. This is consistent with the results of previous researches that aluminum has a significant role in reducing the corrosion rate of alloy steel in seawater [18]. Furthermore, Figure 1 shows the relationships of the Al content (wt. %) and corrosion rate of the steel specimens in the 36.28 g/L NaCl solution, which revealed that the Al content (wt. %) and corrosion rate exhibit a negative linear relationship: \( V = -1.3667\text{Al % (wt. %)} +1.9691 \).
**Figure 1.** The relationship of Al (wt%) and corrosion rate of steel specimens in 35.0 mg/L NaCl solution.

**Figure 2.** Polarization curves (a-c) and the relationship of Al (wt%) and $i_{corr}$ (d) of steel specimens in NaCl solutions at different pHs.
3.2 Polarization curves study

Figure 2 displays the polarization curves of the three aluminum-bearing steel electrodes in NaCl solutions with different acidities/basicities. The polarization curves of the anodes exhibit a similar polarization profile, which suggests the same anodic electrochemical interaction mechanism of aluminum-bearing steel. With increasing anodic potential, all the corrosion current densities had two potential areas; at these two potential intervals, their corrosion current densities increased very little as the potential increased, which suggests that two passive film(s) formed on the electrode surface and hindered the steel dissolution rate.

The detailed polarization kinetics and thermodynamic parameters of corrosion current density ($i_{\text{corr}}$) and corrosion potential ($E_{\text{corr}}$) were dependent on Tafel extrapolation [19] and are listed in Table 3. When the NaCl electrolyte contains the same pH of 5.0, 7.0 or 9.0, specimens 100D, 100E and 100F had a larger concentration of Al (wt. %), which caused smaller corrosion current densities. In the NaCl solution with a pH of 5.0, when the Al content (wt. %) increased from 0.430 to 0.750, the corrosion ($i_{\text{corr}}$) of the steel electrode decreased from 3.251×10^{-4} to 3.229×10^{-4} µA·cm^{-2} and then to 3.188×10^{-4} A·cm^{-2} when the Al (wt. %) was further increased to 0.970. The results showed that increasing the concentration of Al inhibited steel corrosion, which agrees with Wang et al point of view [20]. He believes that the addition of alloying elements, Cr and Al, inhibits the occurrence of corrosion reaction, thus reducing the $i_{\text{corr}}$. The relationships of Al content (wt. %) and $i_{\text{corr}}$ for the three steel specimens in the NaCl solutions with different pH values are shown in Table 3, which also confirmed that the A1 content (wt. %) and the corrosion rate exhibit a negative linear relationship:

$$i_{\text{corr}} = -0.1132\text{Al }\% + 3.3038 \ (\text{pH 5.0}), \ i_{\text{corr}} = -0.3721\text{Al }\% + 2.1843 \ (\text{pH 7.0}) \ \text{and} \ i_{\text{corr}} = -1.4828\text{Al }\% + 2.627 \ (\text{pH 9.0})$$

All these results corresponded with the corrosion weight gain experiment results.

The inhibition efficiencies ($\eta$) can be calculated based on the following equation:

$$\eta = (i_{\text{corr}} - i_{\text{corr}}^0) / i_{\text{corr}}^0 \ [21], \ \text{where} \ i_{\text{corr}}^0 \ \text{and} \ i_{\text{corr}} \ \text{are the initial and the subsequent corrosion current densities, respectively.}$$

Figure 3 shows the inhibition efficiency $\eta_{\text{Al}}$ of aluminum-bearing steel at different concentrations of Al (wt. %). In the NaCl solutions with the same acidities/basicities, larger Al contents had better inhibition efficiencies. When the NaCl solution was acidic (pH 5.0), increases in the Al content (wt. %) from 0.430 to 0.750 or to 0.970 only caused a slight increase in the inhibition efficiency, whereas for the basic NaCl solution, a slight increase in Al (wt. %) caused a great inhibition efficiency: when the concentration of Al (wt. %) increased from 0.430 to 0.750, the inhibition efficiency increased to 25.87, and reached 39.71 when the Al concentration (wt. %) was 0.97.

Corrosion potential ($E_{\text{corr}}$) is a considerable parameter to assess the electrochemical corrosion behavior of materials. Generally speaking, the more positive corrosion potential of material, the better corrosion resistance. As Table 3 shows, at an identical pH value, increasing the content of Al (wt. %) resulted in the corrosion potential shifting to a more positive value; for the same steel specimen, the larger pH value creates a positive corrosion potential. All these data suggest that the aluminum-bearing steel had better corrosion resistance at larger Al contents (wt. %) or when the pH value of the NaCl solution was larger, and these results correspond with those of the corrosion current densities.
Table 3. Polarization parameters of the samples in NaCl solution

<table>
<thead>
<tr>
<th>Sample</th>
<th>pH 7.0</th>
<th></th>
<th>pH 9.0</th>
<th></th>
<th>pH 5.0</th>
<th></th>
</tr>
</thead>
<tbody>
<tr>
<td></td>
<td>$i_{corr}$ (A/cm²)</td>
<td>$E_{corr}$ (mV)</td>
<td>$\eta_{Al}$ (%)</td>
<td>$i_{corr}$ (A/cm²)</td>
<td>$E_{corr}$ (mV)</td>
<td>$\eta_{Al}$ (%)</td>
</tr>
<tr>
<td>100D</td>
<td>3.251×10⁻⁴</td>
<td>-443.4</td>
<td>-</td>
<td>2.011×10⁻⁴</td>
<td>-440.9</td>
<td>-</td>
</tr>
<tr>
<td>100E</td>
<td>3.229×10⁻⁴</td>
<td>-441.8</td>
<td>0.68</td>
<td>1.938×10⁻⁴</td>
<td>-435.5</td>
<td>3.63</td>
</tr>
<tr>
<td>100F</td>
<td>3.188×10⁻⁴</td>
<td>-439.4</td>
<td>1.94</td>
<td>1.804×10⁻⁴</td>
<td>-433.9</td>
<td>10.29</td>
</tr>
</tbody>
</table>

Figure 3. The inhibition efficiencies of aluminium-bearing steel at different concentration of Al.

Figure 4. Nyquist impedance spectra (a-c) and equivalent circuit (d) for the steel specimens in NaCl solution at different pHs.

3.3 Electrochemical impedance spectroscopy study

Figure 4 present the Nyquist plots for the steel specimens in NaCl solutions with different pH values. The Nyquist plots were composed of three capacitive loops, regardless of the pH of the NaCl solution or the concentration of Al (wt. %). The loop at high frequencies is attributed to the protective outer Al and Cr oxide layer. The second capacitive loop at moderate frequencies is related to the passive properties of the inner iron oxide and hydroxyl oxidize iron layer. The detailed characteristics of the
passive films were confirmed via SEM and Raman spectral analyses. The loop at low frequencies is related to the double layer between the aluminum-bearing steel and the outer Helmholtz plane. The electrochemical equivalent circuit (EEC) shown in Figure 4 (d) was used to model the steel/electrolyte interface, which is often used for two passive films, or adsorption and/or insertion processes [22, 23]. In this Figure 4 (d), $R_s$ is the ohmic resistance of the solution, $R_{dl}$ is the charge transfer resistance of ions through the double layer, $R_{olf}$ and $R_{ilf}$ are the passive film resistances of the outer and inner surface film, respectively. $CPE_{dl}$, $CPE_{olf}$ and $CPE_{ilf}$ are the constant phase elements, which are used to replace the charge transfer capacitance at the double layer and the passive film capacitance of the outer layer and the inner layer, respectively. Table 4 shows the impedance parameters and fitting results gained by fitting the EIS data to the EEC.

Comparing the steel electrochemical parameters at different contents of Al (wt. %), we can find out that whether the electrolyte was acidic (pH 5.0), neutral (pH 7.0) or alkali (pH 9.0), when the content of Al (wt. %) increased, the values of $R_{dl}$, $R_{olf}$ and $R_{ilf}$ were all increased. The larger charge transforms resistance ($R_{Q}$) meant that ions have more difficulty transforming at the double layer, and the larger outer and inner layer passive film resistances implied a tighter passive film. All these results are consistence with the polarization results, which found that, for different steel specimens, the specimen that had a larger Al content (wt. %) would have better anticorrosion characteristics in a NaCl solution of the same pH. The results of the experiment are similar to the previous studies. Wang et al. [20] deems that when the Al content of steel was increased, the polarization resistance from EIS also increase. Nishimura [15] found that the corrosion resistance of Al-bearing steel was much higher than carbon steel by EIS method.

In addition, for these specimens, the $R_{dl}$ value was always much larger than the $R_{olf}$ value at the same NaCl solution, which indicates that the inner layer films were the main passive factor.

| Table 4. Model parameters for equivalent circuit of Figure 4 (d) |
|------------------------|------------------------|------------------------|------------------------|------------------------|------------------------|------------------------|------------------------|------------------------|
| NaCl solution          | Sample number          | $CPE_{dl}$ ($\frac{Y_d}{\Omega \cdot \text{cm}^2}$) | $n$ | $C_{dl}$ ($\frac{F}{\text{cm}^2}$) | $R_{dl}$ ($\Omega \cdot \text{cm}^2$) | $CPE_{olf}$ ($\frac{Y_d}{\Omega \cdot \text{cm}^2}$) | $n$ | $C_{olf}$ ($\frac{F}{\text{cm}^2}$) | $R_{olf}$ ($\Omega \cdot \text{cm}^2$) | $CPE_{ilf}$ ($\frac{Y_d}{\Omega \cdot \text{cm}^2}$) | $n$ | $C_{ilf}$ ($\frac{F}{\text{cm}^2}$) | $R_{ilf}$ ($\Omega \cdot \text{cm}^2$) | $X^2$ |
|------------------------|------------------------|------------------------|------------------------|------------------------|------------------------|------------------------|------------------------|------------------------|------------------------|------------------------|------------------------|------------------------|------------------------|
| pH 5.0                 | 100D                   | 3.312E-3               | 0.644                | 2.317E-3               | 158.1                  | 5.95E8                 | 1.0000                 | 5.95E8                 | 4.06                   | 9.65E3                 | 0.6995                 | 1.141E-2               | 152.6                  | 1.53E-4                |
|                       | 100E                   | 2.640E-3               | 0.6805               | 2.108E-3               | 234.6                  | 3.185E8                | 1.0000                 | 3.185E8                | 5.95                   | 6.05E3                 | 0.7081                 | 8.423E3               | 368.4                  | 4.64E-4                |
|                       | 100F                   | 2.157E-3               | 0.7294               | 2.012E-3               | 384.4                  | 2.748E6                | 0.5714                 | 7.253E4                | 6.17                   | 5.03E3                 | 0.6857                 | 8.18E3                | 574.2                  | 1.84E-4                |
| pH 7.0                 | 100D                   | 1.832E-3               | 0.7537               | 1.358E-3               | 218.2                  | 3.617E2                | 0.7447                 | 3.168E2                | 18.8                   | 1.888E2                | 0.6974                 | 3.952E-2              | 290.7                  | 4.78E-4                |
|                       | 100E                   | 1.382E-3               | 0.7843               | 1.141E-3               | 360.8                  | 1.870E3                | 0.7551                 | 6.704E4                | 22.6                   | 1.373E2                | 0.7056                 | 2.658E2              | 354.9                  | 3.64E-4                |
|                       | 100F                   | 1.230E-3               | 0.7994               | 1.101E-3               | 522.2                  | 1.620E3                | 0.8066                 | 7.724E4                | 28.1                   | 1.079E2                | 0.7325                 | 1.865E2              | 415.0                  | 6.13E-4                |
| pH 9.0                 | 100D                   | 1.617E-3               | 0.7513               | 1.162E-3               | 228.0                  | 1.084E2                | 0.6901                 | 6.096E3                | 25.6                   | 1.693E3                | 0.7638                 | 1.538E-3             | 432.7                  | 2.76E-4                |
|                       | 100E                   | 1.344E-3               | 0.7822               | 1.137E-3               | 408.6                  | 1.975E3                | 0.7846                 | 1.165E3                | 74.0                   | 1.374E3                | 0.7662                 | 1.198E3             | 464.2                  | 1.96E-4                |
|                       | 100F                   | 9.651E-4               | 0.7984               | 9.921E-4               | 1156                   | 1.724E3                | 0.8120                 | 1.099E3                | 82.9                   | 1.299E3                | 0.7701                 | 1.14E4             | 503.6                  | 3.57E-4                |

When the steel specimen (100D, 100E or 100F) was immersed in different NaCl solutions with different pH values. As the NaCl solution pH increased from 5.0 to 9.0, the outer and inner passivation film resistances of the samples $R_{olf}$ and $R_{ilf}$ were all increased, and their respective capacitances were all decreased, which suggests that the passivation films had stronger protective effects against steel specimen dissolution. Especially for the 100F specimen, the increased resistance and decreased capacitance changed more remarkably than those of the other specimens. All these results revealed that
increasing the pH is advantageous for aluminum-bearing steel anticorrosion behaviors, especially for specimens with larger Al concentrations. The conclusions were in accordance with those of the polarization results.

Figure 5. SEM images were magnified 1000 times for steel samples exposure to NaCl solution. (a: 100D, pH5.0; b: 100D, pH7.0; c: 100D, pH9.0; d: 100E, pH5.0; e: 100E, pH7.0; f: 100E, pH9.0; g: 100F, pH5.0; h: 100F, pH7.0; i: 100F, pH9.0)

3.4 SEM and Raman spectral analyses

Figure 5 shows the SEM images of the corroded 100D, 100E and 100F surfaces after immersion in NaCl solutions with different pH values for 15 days. It is clear from the images that all the steel samples have experienced severe corrosion. Particularly, at the same NaCl solution (pH 5.0, 7.0, or 9.0), in sequential order from 100D to 100E to 100F, had smaller corroded surfaces and smaller corrosion holes, which indicates that the steel sample that has a smaller Al content (wt. %) had more severe corrosion. In the same steel sample, 100D, 100E or 100F, when the NaCl solution pH values increased, the steel sample had a smaller corroded surface and smaller corrosion, which means that higher alkalinity inhibited the sample corrosion. These results corresponded with the electrochemical results, which found that a larger content of Al (wt. %) or larger value of pH inhibited aluminum-bearing steel corrosion. The
EDS spectra of the three aluminum-bearing steel specimens in the NaCl solutions with pH values of 7.0 are listed in Table 5. The results revealed that oxygen participated in the interaction and that its content in the three specimens decreased in turn (wt. % 100D < 100E < 100F); compared with the pristine aluminum-bearing steel, the content of Al, especially Cr (wt. %) obviously increased. All these data confirmed that aluminum-bearing steel anticorrosion effects increased with increasing Al content.

Figures S1-S4 show the X-ray mapping of O, Al, Cr and Mn after the aluminum-bearing steel samples were corroded in the NaCl solution for 15 days. With decreasing Al content (wt. %) of the aluminum-bearing steel or decreasing pH value of the NaCl solution, we observed a deficiency of Al and Cr, and the accumulations of O and Fe were more obvious. The Al and Cr concentrations in the oxide film of pitting corrosion were lower than the surroundings for Al and Cr diffused into the solution by ions, whereas the O and Fe concentrations in the oxide film of pitting corrosion were higher than the surroundings for the O and Fe precipitated oxidation reactions at the surface.

Figure 6 shows the Raman spectra of the steel samples after corrosion in NaCl solution for 15 days. After the steel samples were corroded for 15 days, before ultrasonic washing (Figure 6 (a)), the Raman spectra of the 100D, 100E and 100F samples in NaCl solutions with different pH values exhibited five Raman peaks near 250, 378, 524, 650-650 and 1307 cm\(^{-1}\). The Raman peak at 378 cm\(^{-1}\) was the feature of a structure for the Al\(_2\)O\(_3\) substances [24]. The Raman peak at 524 cm\(^{-1}\) was assigned to the species of chromium oxide Cr\(_2\)O\(_3\) [25]. The Raman peaks at 250 cm\(^{-1}\) [26-28], 650-660 cm\(^{-1}\) [27, 29, 30] and 1307 cm\(^{-1}\) [29, 30] were assigned to the species of \(\gamma\)-FeOOH.

After ultrasonication, the peaks at 378 cm\(^{-1}\) and 524 cm\(^{-1}\) disappeared in the spectra of the steel samples (Figure 6 (b)), which indicates that Al\(_2\)O\(_3\) and Cr\(_2\)O\(_3\) were all cleared. Three new peaks rose at 219, 282 and 395 cm\(^{-1}\) and 524 cm\(^{-1}\) and in some samples, the peak at 1307 cm\(^{-1}\) shifted to 1320 cm\(^{-1}\). The Raman peaks at 219 and 282 cm\(^{-1}\) were assigned to the species of iron oxide \(\alpha\)-Fe\(_2\)O\(_3\) [31], and the Raman peaks at 395 and 1320 cm\(^{-1}\) were attributed to the species of \(\gamma\)-Fe\(_2\)O\(_3\) [26]. The results revealed that the corrosion products Al\(_2\)O\(_3\) and Cr\(_2\)O\(_3\) should be covered as outer films and hence can easily be cleared, which is consistent with the potentiodynamic curves and EIS measures results.

**Table 5.** EDS elemental analysis (wt%) of steel samples after 20 days exposure in NaCl

<table>
<thead>
<tr>
<th>Element</th>
<th>100D</th>
<th>100E</th>
<th>100F</th>
</tr>
</thead>
<tbody>
<tr>
<td>O</td>
<td>15.04</td>
<td>9.89</td>
<td>7.48</td>
</tr>
<tr>
<td>Al</td>
<td>0.10</td>
<td>0.58</td>
<td>1.13</td>
</tr>
<tr>
<td>Cr</td>
<td>2.33</td>
<td>4.76</td>
<td>6.73</td>
</tr>
<tr>
<td>Fe</td>
<td>81.44</td>
<td>80.64</td>
<td>78.30</td>
</tr>
<tr>
<td>Mn</td>
<td>0.34</td>
<td>0.59</td>
<td>1.02</td>
</tr>
<tr>
<td>Si</td>
<td>0.75</td>
<td>0.30</td>
<td>0.13</td>
</tr>
<tr>
<td>C</td>
<td>-</td>
<td>3.22</td>
<td>3.32</td>
</tr>
<tr>
<td>Mo</td>
<td>-</td>
<td>-</td>
<td>0.31</td>
</tr>
</tbody>
</table>
3.5 Oxidation mechanism of steel (containing Al) in NaCl solution

By summarizing the results from in situ electrochemical analyses and surface measurements, a reasonable corrosion mechanistic pathway for aluminum-bearing steel was suggested as follows. During the aluminum-bearing steel self-corrosion progress, the metal elements, Cr, Al and Fe, acted as anodes and were oxidized.

\[
\begin{align*}
\text{Cr} & \rightarrow \text{Cr}^{3+} + 3e^- \quad (2) \\
\text{Al} & \rightarrow \text{Al}^{3+} + 3e^- \quad (3) \\
\text{Fe} & \rightarrow \text{Fe}^{2+} + 2e^- \quad (4)
\end{align*}
\]

Oxygen acted as an oxidizing agent, and the reduction reaction took place as a cathodic reaction [32].

\[
\text{O}_2 + 2\text{H}_2\text{O} + 4e^- \rightarrow 4\text{OH}^- \quad (5)
\]

Furthermore, the dissolution of chromium is thought to take place as reaction (6) [33], the dissolution of aluminum is expected to occur as reaction (7) [15], and Fe\(^{2+}\) will also transform into iron oxide (such as Fe\(_2\)O\(_3\)):

\[
\begin{align*}
2\text{Cr}^{3+} + 3\text{H}_2\text{O} + 3e^- & \rightarrow \text{Cr}_2\text{O}_3 \quad (6) \\
2\text{Al}^{3+} + 3\text{H}_2\text{O} + 3e^- & \rightarrow \text{Al}_2\text{O}_3 \quad (7)
\end{align*}
\]

According to the thermodynamic data [34, 35], the heat of formation values of Al\(_2\)O\(_3\), Cr\(_2\)O\(_3\) and Fe\(_2\)O\(_3\) at 25°C are -1669.8, -1058.58 and -824.60 kJ mol\(^{-1}\), respectively. Hence, Al and Cr preferentially oxidize before Fe, and their oxides act as outer films, which correspond with the above Raman results. Fe\(^{2+}\) will also transform in the Al and Cr outer film, which is not completely isolated from oxygen and water molecules, and Fe\(^{2+}\) can further interact and lead to the formation of a thin unstable colloidal hydroxyl salt layer called GreenRust (GR), 3Fe(OH)\(_2\)-Fe(OH)\(_2\)Cl\(-n\)H\(_2\)O, from the action of the oxygen and chloride effect [36-38].

\[
\begin{align*}
\text{Fe}^{2+} + 2\text{OH}^- & \rightarrow \text{Fe(OH)}_2 \quad (8) \\
7\text{Fe(OH)}_2 + \text{Fe}^{2+} + 2\text{Cl}^- + 1/2\text{O}_2 + (2n+1)\text{H}_2\text{O} & \rightarrow 2[3\text{Fe(OH)}_2\cdot\text{Fe(OH)}_2\text{Cl}\cdot n\text{H}_2\text{O}] \quad (9)
\end{align*}
\]
Generally, the GreenRust $[\text{Fe}(\text{H}_2\text{O})_x]\text{Cl}_2$ is not stable and undergoes further transformation to $\gamma$-FeOOH (lepidocrocite) via the pathway (10) [33, 39, 40] and even to $\gamma$-Fe$_2$O$_3$ and $\alpha$-Fe$_2$O$_3$ via pathways (11) and (12). The above transformation from $\gamma$-Fe$_2$O$_3$ to $\alpha$-Fe$_2$O$_3$ is impossible under thermodynamic criteria, FeOOH is more thermodynamically stable than $\gamma$-Fe$_2$O$_3$. In addition, $\alpha$-Fe$_2$O$_3$ cannot be formed under in situ conditions [40]. However, when exposed to a dry atmosphere, the formation of $\alpha$-Fe$_2$O$_3$ is earthly via a dehydration reaction, and the reaction proceeds through $\alpha$-FeOOH or $\gamma$-Fe$_2$O$_3$ [40-42]. The ex situ Raman analysis confirmed the formation of $\alpha$-Fe$_2$O$_3$.

$\begin{align*}
3\text{Fe(OH)}_2\cdot\text{Fe(OH)}_2\text{Cl} \cdot n\text{H}_2\text{O} & \rightarrow [\text{Fe(H}_2\text{O})_x]\text{Cl}_2 \rightarrow \gamma\text{-FeOOH}, \text{FeOCl} + \text{H}_2\text{O} \rightarrow \gamma\text{-FeOOH (10)} \\
8\gamma\text{-FeOOH} & \rightarrow 4\gamma\text{-Fe}_2\text{O}_3 + 4\text{H}_2\text{O} \rightarrow \alpha\text{-Fe}_2\text{O}_3 + 4\text{H}_2\text{O} \quad (11) \\
2\gamma\text{-FeOOH} & \rightarrow 2\alpha\text{-FeOOH} \rightarrow \alpha\text{-Fe}_2\text{O}_3 + \text{H}_2\text{O} \quad (12)
\end{align*}$

According to the above analysis, the corrosion mechanism of aluminum-bearing steel in NaCl solution is shown in Figure 7.

**Figure 7.** The oxidation mechanism of aluminium-bearing steel in NaCl solution.

### 4. CONCLUSIONS

The effects of the Al content on the corrosion behaviors of aluminum-bearing steels in NaCl solutions were researched by electrochemical measurements and surface analyses. The following conclusions can be drawn:

1. There is a negative linear relationship between the Al content (Al%) and corrosion rate ($V$), which is expressed as $V = -1.3667\text{Al} \% \ (\text{wt.}) + 1.9691$ in the investigated conditions (Al content between 0.430 and 0.970).

2. The polarization curve studies indicated that aluminum-bearing steel corrosion had two passive potential intervals. Increasing the concentration of Al or increasing the pH of the NaCl solutions...
causes the corrosion potential to become more positive and is advantageous for aluminum-bearing steel anticorrosion behaviors.

(3) The EIS studies showed that the dominant anticorrosion effect comes from the inner layer film, but a larger content of Al causes a larger charge transform resistance and larger outer and inner passive resistances, which results in better anticorrosion behaviors.

(4) The SEM and Raman spectral analyses confirmed that the outer layer film was composed of Al₂O₃ and Cr₂O₃, and the inner layer film was composed of lepidocrocite (γ-FeOOH) regardless of whether the NaCl solution was faintly acidic/alkali or neutral. γ-FeOOH is unstable and can transform to α-Fe₂O₃ and γ-Fe₂O₃ when exposed to air.

SUPPLEMENTARY INFORMATION

Figure S1. EDS Analysis of Element Al in Steel Samples Exposed to NaCl Solution.
(a: 100D, pH5.0; b: 100D, pH7.0; c: 100D, pH9.0; d: 100E, pH5.0; e: 100E, pH7.0; f: 100E, pH9.0; g: 100F, pH5.0; h: 100F, pH7.0; i: 100F, pH9.0)
**Figure S2.** EDS Analysis of Element Fe in Steel Samples Exposed to NaCl Solution.

(a: 100D, pH5.0; b: 100D, pH7.0; c: 100D, pH9.0; d: 100E, pH5.0; e: 100E, pH7.0; f: 100E, pH9.0; g: 100F, pH5.0; h: 100F, pH7.0; i: 100F, pH9.0)
Figure S3. EDS Analysis of Element Cr in Steel Samples Exposed to NaCl Solution.
(a: 100D, pH5.0; b: 100D, pH7.0; c: 100D, pH9.0; d: 100E, pH5.0; e: 100E, pH7.0; f: 100E, pH9.0; g: 100F, pH5.0; h: 100F, pH7.0; i: 100F, pH9.0)
Figure S4. EDS Analysis of Element O in Steel Samples Exposed to NaCl Solution.
(a: 100D, pH5.0; b: 100D, pH7.0; c: 100D, pH9.0; d: 100E, pH5.0; e: 100E, pH7.0; f: 100E, pH9.0; g: 100F, pH5.0; h: 100F, pH7.0; i: 100F, pH9.0)

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References