Reaction/Diffusion at Electrode/Solution Interfaces: The EC₂ Reaction

Michael E G Lyons^{*} Physical and Materials Electrochemistry Laboratory, School of Chemistry, University of Dublin, Trinity College, Dublin 2, Ireland. *E-mail: <u>melyons@tcd.ie</u>

Received: 6 July 2009 / Accepted: 15 August 2009 / Published: 25 August 2009

A closed form analytical expression is derived for the normalized current versus potential response expected for a rotating disc electrode in which an initial fast electron transfer reaction is followed by a homogeneous electrochemical reaction which exhibits second order kinetics. The effect of the homogeneous reaction on the shape of the voltammetric response curve is calculated.

Keywords: Reaction/diffusion equations; Electrode kinetics; EC reactions.

1. INTRODUCTION

In this short paper we present a generalized theoretical analysis for second order EC processes at a rotating disc electrode. The analysis of diffusion processes with concurrent chemical reaction is well established in electrochemistry [1]. However much of the published work has concentrated on the coupling between reactant diffusion and first order homogeneous chemical reaction and the mathematical analysis of the CE and EC reaction schemes [2,3] is well established. However little work has been reported on reactant diffusion coupled with second order homogeneous reactant kinetics. More than 30 years ago Ulstrup [4] examined second order kinetic processes at a rotating disc electrode and derived a simple expression for the limiting current for the case where an intermediate undergoes a fast disproportionation under steady state conditions. More recently Compton and co-workers [5] examined coupled diffusion and second order kinetics at a rotating disc electrode and obtained, via numerical analysis, working curves for the expected current versus potential response. Bartlett and Eastwick-Field [6] derived approximate analytical expressions for the limiting current at the rotating disc electrode for the ECE mechanism where the chemical step is irreversible. The situation corresponding to both pseudo-first order and second order kinetics was examined. Feldberg and co-workers [7] carried out a digital simulation of a second order ECE dimerization reaction at a rotating disc electrode.

In the present paper we describe a simple analysis of the EC_2 reaction scheme in which an electro-generated intermediate reacts via second order kinetics.

2. THEORETICAL MODEL

2.1 Model setup and general considerations

We consider the following reaction scheme.

$$\begin{array}{c} A \xrightarrow{\mp n e^{-}} & B \\ 2B \xrightarrow{k} & P \end{array} \tag{1}$$

In this scheme A denotes a stable species in solution undergoing an oxidation or reduction reaction at a support electrode to an unstable intermediate species B which subsequently decomposes via a chemical transformation within the diffusion layer to a product species P via second order kinetics. The rate of the latter reaction is quantified by the bimolecular rate constant k (units: $cm^3mol^{-1}s^{-1}$).

If steady state behaviour is assumed then the pertinent reaction diffusion equations are given by

$$D\frac{d^{2}a}{dx^{2}} = 0$$

$$D\frac{d^{2}b}{dx^{2}} - 2kb^{2} = 0$$
(2)

In the latter expressions a and b denote the concentrations of species A and B at any distance x from the electrode surface and we have assumed for simplicity that all species have identical diffusion coefficients so that $D_A = D_B = D$. We further assume that diffusion is Ficksian and planar and that x represents the distance normal from the electrode surface. We have also assumed that convection terms can be nglected in the transport equations. This assumption is well established [8].

We introduce the following scaling parameters which serve to make the reaction/diffusion equations dimensionless:

$$u = \frac{a}{a^{\infty}} \quad v = \frac{b}{a^{\infty}} \quad \chi = \frac{x}{\delta} \tag{3}$$

where a^{∞} denotes the bulk concentration of reactant species A and δ represents the Nernst Diffusion Layer thickness, which for a rotating disc electrode is given by [9]:

$$\delta = 0.64 \nu^{1/6} D^{1/3} W^{-1/2} \tag{4}$$

where ν denotes the kinematic viscosity of the solution and W is the electrode rotation speed (units: Hz). We finally introduce a reaction/diffusion parameter γ such that

$$\gamma = \frac{k\delta^2 a^{\infty}}{D} = \frac{k\delta a^{\infty}}{D/\delta} = \frac{f_K}{f_D}$$
(5)

This parameter represents the balance between homogeneous chemical reaction (quantified in terms of a kinetic flux f_K) and diffusion (expressed in terms of a diffusive flux f_D).

The system of reaction/diffusion equations therefore adopts the following adimensional form

$$\frac{d^2 u}{d\chi^2} = 0$$

$$\frac{d^2 v}{d\chi^2} - 2\gamma v^2 = 0$$
(6)

The boundary conditions defining the problem are given by

$$\chi = 0 \quad u_0 = v_0 \exp\left[-\xi\right]$$

$$\chi = 0 \quad \left(\frac{du}{d\chi}\right)_0 + \left(\frac{dv}{d\chi}\right)_0 = 0$$

$$\chi = 1 \quad u = 1 \quad v = 0$$
(7)

The first boundary condition pertains to the region immediately adjacent to the electrode surface and implies that the A/B redox transformation is kinetically facile and Nernstian. In this expression the parameter ξ denotes a normalised potential and is defined as

$$\xi = \frac{F}{RT} \left(E - E^0 \right) = \theta - \theta^0 \tag{8}$$

We also introduce a normalised current Ψ such that

$$\Psi = \frac{f_{\Sigma}}{f_D} = \frac{f_{\Sigma}}{Da^{\infty}/\delta}$$
(9)

In the latter expression f_{Σ} denotes the flux arising at any applied potential E and f_D represents the diffusion limited flux which is observed at elevated potentials.Note that the relationship between reaction flux f_{Σ} and current *i* is given by

$$f_{\Sigma} = \frac{i}{nFA} \tag{10}$$

where n, F and A denote the number of electrons transferred, the Faraday constant and the electrode geometric area respectively. Hence the normalised current is given by

$$\Psi = \left(\frac{du}{d\chi}\right)_0 = -\left(\frac{dv}{d\chi}\right)_0 \tag{11}$$

Note that the third statement presented in eqn.7 assumes that the concentration of the electrogenerated product species B at the edge of the diffusion layer when $x = \delta$ is zero. This assumption will be valid provided that B decomposes rapidly via second order reaction and so the bimolecular rate constant k will be very much larger than the rate of diffusion of B through the diffusion layer. Hence the boundary condition will be valid when the reaction/diffusion parameter γ is large.

2.2. Solution of the reaction/diffusion equations

We now solve the system of equations presented in eqn.6 subject to the boundary conditions outlined in eqn.7 to obtain an expression for the steady state voltammogram.

The first expression presented in eqn.6 may be directly integrated to produce

$$u(\chi) = A\chi + B \tag{12}$$

The constants of integration A and B are readily shown via application of the boundary conditions to be $A = \left(\frac{du}{d\chi}\right)_0 = \Psi = 1 - u_0$, $B = u_0$. Hence the reactant concentration profile within the diffusion layer

is linear and takes the form

$$u(\chi) = u_0 + (1 - u_0)\chi$$
(13)

A full integration of the v-expression presented in eqn.6 can be accomplished via the following idea. We set $\rho = \frac{dv}{d\chi}$ and so $\frac{d^2v}{d\chi^2} = \frac{d\rho}{d\chi} = \frac{d\rho}{dv}\frac{dv}{d\chi} = \rho\frac{d\rho}{dv}$ and the second expression in eqn.6 reduces to $\rho\frac{d\rho}{dv} - 2\gamma v^2 = 0$ (14)

Integrating the latter expression yields:

$$p_{1}^{2} - p_{0}^{2} = \frac{4\gamma}{3} \left(v_{1}^{3} - v_{0}^{3} \right)$$

$$p_{0}^{2} = \left(\frac{4\gamma}{3} \right) v_{0}^{3}$$
(15)

In performing the latter integration we specifically assume that at the edge of the diffusion layer at $\chi = 1$, $\rho_1 = \left(\frac{dv}{d\chi}\right)_1 \cong 0$, $v_1 = 0$. This assumption will be valid for large values of the reaction/diffusion parameter. Noting that $\rho_0^2 = \Psi^2$ we immediately obtain the following useful result

$$v_0 = \left\{\frac{3}{4\gamma}\right\}^{1/3} \Psi^{2/3}$$
(16)

From the Nernst equation we note that

$$v_0 = u_0 \exp[\xi] = (1 - \Psi) \exp[\xi]$$
⁽¹⁷⁾

Equating the expressions for v_0 outlined in eqn.16 and eqn.17 we obtain the following expression defining the current response

$$1 - \Psi = \lambda \Psi^{2/3} \tag{18}$$

Where we have set

$$\lambda(\gamma,\xi) = \left\{\frac{3}{4\gamma}\right\}^{1/3} \exp\left[-\xi\right]$$
(19)

Alternatively we write

$$\left(\Psi^{1/3}\right)^3 + \lambda \left(\Psi^{1/3}\right)^2 - 1 = 0 \tag{20}$$

This is a cubic equation in $\Psi^{1/3}$. We note immediately that as the potential is driven to extreme values $\xi \to \infty$, $\exp[-\xi] \to 0$ and so $\lambda \to 0$ and from eqn.18 we note that $\Psi \to 1$, $f_{\Sigma} \to f_D$ and the diffusion controlled plateau region is reached as we would expect. Furthermore when the reaction/diffusion parameter γ is large signifying that the homogeneous reaction flux for the dimerization is much larger than the diffusive flux then again the reaction is under net diffusion control and again $\Psi \to 1$.

2.3. Evaluation of the steady state voltammetric curve

One general form [9] of a cubic equation is given by the so called normal form:

$$x^3 + a_1 x^2 + a_2 x + a_3 = 0 \tag{21}$$

In the latter expression we have set the coefficient $a_0 = 1$ without loss of generality, and the coefficients a_k , k = 1,...3 define constant coefficients. If we define the following quantities:

$$Q = \frac{3a_2 - a_1^2}{9}$$

$$R = \frac{9a_1a_2 - 27a_3 - 2a_1^3}{54}$$

$$S = \left\{ R + \sqrt{\Delta} \right\}^{1/3}$$

$$T = \left\{ R - \sqrt{\Delta} \right\}^{1/3}$$
(22)

We note that the discriminant Δ is given by:

$$\Delta = Q^3 + R^2 \tag{23}$$

The cubic will admit the following real and complex roots provided that $\Delta > 0$:

$$x_{1} = S + T - \frac{a_{1}}{3}$$

$$x_{2} = -\frac{(S+T)}{2} - \frac{a_{1}}{3} + \frac{\sqrt{3}}{2}(S-T)i$$

$$x_{3} = -\frac{(S+T)}{2} - \frac{a_{1}}{3} - \frac{\sqrt{3}}{2}(S-T)i$$
(24)

And we choose the single real root as being physically meaningful.

For the present problem we compare eqn.20 and eqn.21 and identify $a_1 = \lambda$, $a_2 = 0$, $a_3 = -1$. Hence we note that $Q = -\frac{\lambda^2}{9}$, $R = \frac{27 - 2\lambda^3}{54} = \frac{1}{2} - \frac{\lambda^3}{27} = \frac{1}{2} - \left(\frac{\lambda}{3}\right)^3$. Furthermore we note that $Q^3 = -\frac{\lambda^6}{729} = -\lambda^3 \left(\frac{\lambda}{9}\right)^3$, $R^2 = \left(\frac{1}{2} - \frac{\lambda^3}{27}\right)^2 = \frac{1}{4} - \frac{\lambda^3}{27} + \frac{\lambda^6}{729} = \frac{1}{4} - \frac{\lambda^3}{27} + \lambda^3 \left(\frac{\lambda}{9}\right)^3$ and so the discriminant is given by $\Delta = Q^3 + R^2 = \frac{1}{4} - \frac{\lambda^3}{27} = \frac{1}{4} - \left(\frac{\lambda}{3}\right)^3 > 0$. This implies that our analysis will be valid provided that $\lambda < \left(\frac{27}{4}\right)^{1/3} = 1.889$. Using eqn.19 we note that the value of λ depends both on the numerical values of the reaction/diffusion parameter γ and the normalized potential ξ . We can compute the minimum value of normalized potential required to ensure the validity of the condition $\lambda < \lambda_{critical}$ with $\lambda_{critical} = 1.889$ for a given γ value. For normalized potential values more negative than this the discriminant will not be positive. The results of the required computation is presented in table 1 below. This calculation in fact defines a lower bound for the potential which must be applied to ensure that the condition of rapid homogeneous kinetics is met.

Tuble I. Dependence of normalized potential of reaction and an parameter	
γ	$\xi_{\min}(\lambda < \lambda_{critical})$
10	-1.49
100	-2.27
1000	-3.03
10000	-3.80

Table 1. Dependence of normalized potential on reaction/diffusion parameter

Note also that for large values of λ , Δ will be positive since as the normalized potential ξ increases the λ^3 term will decrease and eventually approach zero. We can also show that $S = \left\{\frac{1}{2} - \frac{\lambda^3}{27} + \sqrt{\frac{1}{4} - \frac{\lambda^3}{27}}\right\}^{1/3}$ and also $T = \left\{\frac{1}{2} - \frac{\lambda^3}{27} - \sqrt{\frac{1}{4} - \frac{\lambda^3}{27}}\right\}^{1/3}$ and so the physically meaningful

solution to eqn.20 is:

$$\Psi^{1/3} = \left\{ \frac{1}{2} - \frac{\lambda^3}{27} + \sqrt{\frac{1}{4} - \frac{\lambda^3}{27}} \right\}^{1/3} + \left\{ \frac{1}{2} - \frac{\lambda^3}{27} - \sqrt{\frac{1}{4} - \frac{\lambda^3}{27}} \right\}^{1/3} - \frac{\lambda}{3}$$
(25)

And the expression for the normalized current takes the form:

$$\Psi = \left\{ \left\{ \frac{1}{2} - \left(\frac{\lambda}{3}\right)^3 + \sqrt{\frac{1}{4} - \left(\frac{\lambda}{3}\right)^3} \right\}^{1/3} + \left\{ \frac{1}{2} - \left(\frac{\lambda}{3}\right)^3 - \sqrt{\frac{1}{4} - \left(\frac{\lambda}{3}\right)^3} \right\}^{1/3} - \frac{\lambda}{3} \right\}^3$$
(26)

If we substitute the expression for λ outlined in eqn.19 into eqn.26 we obtain an explicit expression for the normalized current versus potential curve as desired.

Returning to the cubic equation illustrated in eqn.20 we can set $\Psi^{1/3} = Z - \frac{\lambda}{3}$ and hence the cubic transforms to

$$\left(Z - \frac{\lambda}{3}\right)^3 + \lambda \left(Z - \frac{\lambda}{3}\right)^2 - 1 = 0$$
(27)

Which simplifies to

$$Z^3 - \alpha Z - \beta = 0 \tag{28}$$

Where we have set

$$\alpha = \frac{\lambda^2}{3}$$

$$\beta = 1 - \frac{2\lambda^3}{27}$$
(29)

Provided that $27\beta^2 > 4\alpha^3$ then the cubic equation presented in eqn.28 will have one real and two complex roots. Furthermore it can be shown that we can find ϑ such that

$$\cosh\vartheta = \left(\frac{3}{\alpha}\right)^{3/2} \frac{\beta}{2} \tag{30}$$

And we can find the real root given by

$$Z = \frac{2}{\sqrt{3}} \sqrt{\alpha} \cosh\left[\frac{\vartheta}{3}\right]$$

= $\frac{2\lambda}{3} \cosh\left[\frac{\vartheta}{3}\right] = 2\kappa \cosh\left[\frac{\vartheta}{3}\right]$ (31)

We can readily show that

$$\vartheta = \cosh^{-1}\left\{\frac{1-2\kappa^3}{2\kappa^3}\right\} = \ln\left\{\left(\frac{1-2\kappa^3}{2\kappa^3}\right) + \sqrt{\left(\frac{1-2\kappa^3}{2\kappa^3}\right)^2 - 1}\right\}$$
(32)

where we have set

$$\kappa = \lambda/3 = \frac{1}{3} \left\{ \left\{ 3/4\gamma \right\}^{1/3} \exp\left[-\xi\right] \right\}$$
(33)

Hence the normalized current response can be evaluated from

$$\Psi = (Z - \kappa)^3 = \left\{ \kappa \left(2\cosh\left[\frac{\vartheta}{3}\right] - 1 \right) \right\}^3$$
(34)

This is an alternative expression for the normalized current response and can be used to define the voltammetric response when the explicit potential dependence of the κ parameter is inputted via the expression outlined in eqn.33.

We now evaluate the half wave potential. We note that the normalized potential is defined as: $\xi = \frac{F}{RT} (E - E^0) = \theta - \theta^0, \text{ and when } \theta = \theta_{1/2}, \quad \Psi = 1/2. \text{ Hence from eqn.20 we obtain that}$ $\left\{ \left(\frac{1}{2}\right)^{1/3} \right\}^3 + \left\{ \frac{3}{4\gamma} \right\}^{1/3} \exp\left[-\left(\theta_{1/2} - \theta_0\right) \right] \left\{ \frac{1}{2} \right\}^{2/3} = 1. \text{This expression is readily shown to simplify to:}$ $\sum_{n=1}^{\infty} \left[\left(\frac{3}{2}\right)^{1/3} \left(\frac{1}{2}\right)^{2/3} \right] = 1. \text{This expression is readily shown to simplify to:}$

 $\exp\left[-\left(\theta_{1/2}-\theta_{0}\right)\right]\left\{\left(\frac{3}{4\gamma}\right)^{1/3}\left(\frac{1}{2}\right)^{2/3}\right\}=\frac{1}{2}, \text{ and so we obtain on further rearrangement the following}$

expression for the half wave potential:

$$\theta_{1/2} = \theta_0 + \frac{1}{3} \ln 2 + \frac{1}{3} \ln \left\{ \frac{3}{4\gamma} \right\}$$
(35)

We note that since the reaction/diffusion parameter γ is always positive then the term $\ln \{3/4\gamma\} < 0$ and so for an oxidation process, $\theta_{1/2} < \theta_0$ and $\frac{d\theta_{1/2}}{d \ln \gamma} = -\frac{1}{3}$. Hence we predict that the half wave potential should be shifted to more negative values with increasing values of the reaction/diffusion parameter γ . This variation, computed from eqn.35 is presented in figure 1 and in semi-logarithmic format in figure 2. These results are in agreement with data previously reported by Compton and coworkers [5] who attacked the problem using numerical methods.



Figure 1. Variation of $\Delta \theta = \theta_{1/2} - \theta_0$ with reaction/diffusion parameter γ for an EC₂ process computed from eqn.35.

Returning to eqn.14 we can integrate across the width of the diffusion layer to obtain:

$$\int_{0}^{p} p dp = 2\gamma \int_{0}^{v} v^{2} dv$$

$$p^{2} = \frac{4\gamma}{3} \left\{ v^{3} - v_{0}^{3} \right\} + p_{0}^{2}$$
(36)

We recall that $p_0^2 \cong \frac{4\gamma}{3} v_0^3$ and so :

$$p^{2} = \left(\frac{dv}{d\chi}\right)^{2} = \frac{4\gamma}{3}v^{3}$$

$$\frac{dv}{d\chi} = -\sqrt{\frac{4\gamma}{3}}v^{3/2}$$
(37)

Separating the variables and integrating produces the following expression for the concentration profile of the electro-generated reactant species B in the diffusion layer:

$$\frac{1}{\sqrt{\nu}} = \frac{1}{\sqrt{\nu_0}} + \sqrt{\frac{\gamma}{3}}\chi$$
(38)



Figure 2. Presentation of eqn.35 in semi-logarithmic format.

Furthermore since v = 0 $\chi = 1$ then $v_0 = -\frac{3}{\gamma}$ and so the concentration profile is given by $\frac{1}{\sqrt{\nu}} = \sqrt{\frac{\gamma}{3}} \{\chi - 1\}$ (39)

From eqn.15 we also note that

$$p_0 = \left(\frac{dv}{d\chi}\right)_0 = -\left(\frac{du}{d\chi}\right)_0 = -\sqrt{\frac{4\gamma}{3}}v_0^{3/2}$$
(40)

Also we note that

$$\left(\frac{du}{d\chi}\right)_0 = 1 - u_0 = 1 - v_0 \exp\left[-\xi\right]$$
(41)

From eqn. 40 and eqn.41 we immediately obtain

$$\sqrt{\frac{4\gamma}{3}} v_0^{3/2} + \exp\left[-\xi\right] v_0 - 1 = 0$$
(42)

The latter may be written in the following form

$$\left(\sqrt{v_0}\right)^3 + \sqrt{\frac{3}{4\gamma}} \exp\left[-\xi\right] \left(\sqrt{v_0}\right)^2 - \sqrt{\frac{3}{4\gamma}} = 0$$
(43)

The latter expression defines a cubic in $\sqrt{v_0}$ which may also be solved via procedures similar to those outlined earlier in the paper. This approach was adopted by Compton and co-workers [5].

2.4 Extension of analysis to a general mth order homogeneous reaction: the EC_m process.

We now briefly discuss how the analysis developed in the present paper may be extended to a more general reaction sequence in which one has an initial rapid interfacial heterogeneous electron transfer reaction followed by a homogeneous chemical reaction which follows mth order kinetics with a rate constant k.

We focus specific attention on the homogeneous reaction step occurring within the diffusion layer of thickness δ involving the electro-generated reactant in which the reaction stoichiometry is:

$$mB \xrightarrow{k} Products$$

Again the reaction/diffusion equation takes the form:

$$\frac{d^2 v}{d\chi^2} - m\gamma v^m = 0 \tag{44}$$

Where we have defined the reaction/diffusion parameter in this case as:

$$\nu = \frac{k\delta^2}{D} \left(a^{\infty}\right)^{m-1} \tag{45}$$

Proceeding as before we get

$$2\frac{dv}{d\chi}\frac{d^2v}{d\chi^2} = 2m\gamma v^m \frac{dv}{d\chi}$$
(46)

Now again we note that $\frac{d}{d\chi} \left\{ \left(\frac{dv}{d\chi} \right)^2 \right\} = 2 \frac{dv}{d\chi} \frac{d^2 v}{d\chi^2}$ and we also note that $\frac{d}{dv} \left\{ \frac{2m\gamma}{1+m} v^{1+m} \right\} = 2m\gamma v^m \frac{dv}{d\chi}$

hence from eqn.46 we obtain:

$$\int \frac{d}{d\chi} \left\{ \left(\frac{dv}{d\chi} \right)^2 \right\} d\chi = \int \frac{2m\gamma}{(1+m)} v^{1+m} \frac{dv}{d\chi} d\chi$$
(47)

Integrating both sides produces

$$\left(\frac{dv}{d\chi}\right)^2 = \frac{2m\gamma}{(1+m)}v^{1+m} + K$$
(48)

The integration constant K is obtained by appropriate use of the boundary conditions. When

$$\chi = 1$$
 $v = v_1 = 0$ $\frac{dv}{d\chi} = \left(\frac{dv}{d\chi}\right)_1$ and so $K = \left(\frac{dv}{d\chi}\right)_1$. If we can make the further assumption that

 $\left(\frac{dv}{d\chi}\right)_1 \cong 0$ then K =0 and we obtain from eqn.48 that

$$\frac{dv}{d\chi} \cong -\sqrt{\frac{2m\gamma}{(1+m)}} v^{(1+m)/2}$$
(49)

Specifically at $\chi = 0$ the current is given by

$$\Psi = -\left(\frac{dv}{d\chi}\right)_0 = \sqrt{\frac{2m\gamma}{(1+m)}} v_0^{(1+m)/2}$$
(50)

We recall that $u_0 = 1 - \Psi$ hence $u_0 = 1 - \sqrt{\frac{2m\gamma}{(1+m)}} v_0^{(1+m)/2}$. Furthermore from the Nernst equation at the

electrode surface we note $u_0 = v_0 \exp[-\xi]$. Hence we obtain that:

$$-\Psi = v_0 \exp\left[-\xi\right] \tag{51}$$

From eqn.50 we obtain that:

$$v_0 = \left\{\frac{1+m}{2m\gamma}\right\}^{1/(1+m)} \Psi^{2/(1+m)}$$
(52)

Hence from eqn,51 and eqn.52 we obtain the following expression for the current versus potential curve for a mth order reaction:

$$1 - \Psi = \Psi^{2/(1+m)} \left\{ \frac{1+m}{2m\gamma} \right\}^{1/(1+m)} \exp[-\xi]$$
(53)

This expression may be written as:

$$\Psi + \Psi^{2/(1+m)} \exp\left[-\xi^*\right] - 1 = 0 \tag{54}$$

Where we have introduced

$$\xi^* = \xi + \frac{1}{1+m} \ln\left\{\frac{2m\gamma}{1+m}\right\}$$
(55)

This expression is in agreement with a result first proposed by Amatore [12]. Specifically for m = 2 we note that eqn.52 reduces to eqn.16 and eqn.54 transforms to eqn.20 as indeed it should.

3. CONCLUSIONS

In the present paper an analysis of an EC_2 reaction sequence involving a Nernstian interfacial electron transfer reaction followed by a homogeneous dimerization reaction occurring in the diffusion layer is presented. The pertinent reaction-diffusion equations have been formulated and solved under steady state conditions subject to defined boundary conditions. The analysis has enabled an algebraic expression for either the normalized current or the surface concentration of electro-generated reactant

to be formulated in terms of a cubic equation. Two closed form analytical solutions to the cubic have been proposed using standard methodologies. The variation in half wave potential with a characteristic reaction/diffusion parameter has been proposed. Finally the extension of the analysis to an EC_P type process has been demonstrated.

Acknowledgements

This work was supported by Enterprise Ireland (Grant number SC/2003/0049), IRCSET (Grant number SC/2002/0169) and the HEA-PRTLI Programme.

References

- C.P. Andrieux and J.M. Saveant in *Investigation of rates and mechanism of reactions*. Part II. (C.F. Bernasconi, Ed.,), 4th Edition, *Techniques of Chemistry Series*, Vol. VI, Wiley, New York, 1986, Chapter 7, pp. 305-390.
- 2. A.J. Bard, L.R. Faulkner, *Electrochemical Methods: Fundamentals and Applications*, Wiley, New York, 1980, Chapter 11, pp.429-487.
- (a) J. Koutecky and R. Brdicka, Collect. Czech Chem. Commun., 12 (1947) 337; (b) P. Delehay, S. Ora, J. Am. Chem. Soc., 82 (1960) 329; L.H.J. Tong, K. Liang and W.R. Ruby, J. Electroanal. Chem., 13 (1967) 245; Z. Galus, R.N. Adams, J. Electroanal. Chem., 4 (1962) 248.
- 4. J. Ulstrup, *Electrochim Acta.*, 13 (1968) 1717.
- 5. (a) R.G. Compton, D. Mason and P.R. Unwin, J. Chem. Soc. Faraday Trans. I. 84 (1988) 473;
 (b) R.G. Compton, P.R. Unwin, J. Chem. Soc. Faraday Trans. I. 85 (1989) 1821.
- 6. P.N. Bartlett, V. Eastwick-Field, J. Chem. Soc. Faraday Trans. I. 89 (1993) 213.
- 7. L.S. Marcoux, R.N. Adams and S.W. Feldberg, J. Phys. Chem., 73 (1969) 2611.
- 8. W.J. Albery, *Electrode Kinetics*, Clarendon Press, Oxford, 1975, pp.51-53.
- 9. W.J. Albery and M.L. Hitchman, *Ring-Disc Electrodes*, Clarendon Press, Oxford, 1971, p.13.
- 10. H.T. Davis, *Introduction to nonlinear differential and integral equations*, Dover, New York, 1962, pp.194-197.
- 11. M.R. Spiegel, Mathematical Handbook, McGraw Hill, New York, 1968, pp.179-182.
- 12. C. Amatore, in *Organic Electrochemistry*, (H. Lund, M.M. Baizer, Eds.), 3rd Edition, Marcel Dekker, New York, 1991, Chapter 2, pp.11-119.

© 2009 by ESG (<u>www.electrochemsci.org</u>)