Adsorption Behaviour of Cefapirin on Mild Steel in Hydrochloric Acid Solution

Ashish Kumar Singh^{1, 2,*}, Eno E. Ebenso¹, M. A. Quraishi²

¹ Department of Chemistry, School of Mathematical and Physical Sciences, North- West University (Mafikeng Campus), Private Bag X2046, Mmabatho 2735, South Africa

² Department of Applied Chemistry, Institute of Technology, Banaras Hindu University, Varanasi 221 005 (India)

*E-mail: <u>ashish.singh.rs.apc@itbhu.ac.in</u>

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The adsorption behaviour of cefapirin (CFP) on mild steel (MS) in 1 M HCl solution was studied using potentiodynamic polarization, electrochemical impedance spectroscopy (EIS) and weight loss techniques. The surface morphology of the MS after its exposure to 1 M HCl solution with and without 400 ppm CFP was examined using scanning electron microscopy (SEM). The value of activation energy (E_a), Arrhenius factor, enthalpy and entropy for the MS corrosion inhibition and the thermodynamic parameters such as adsorption equilibrium constant (K_{ads}), free energy of adsorption (ΔG_{ads}^0), adsorption heat (ΔH_{ads}^0) and adsorption entropy (ΔS_{ads}^0) values were calculated and discussed. The adsorption behaviour of CFP is experimentally investigated by contact angle measurement on mild steel surface. The hydrophobic character of MS increased with increasing concentration of CFP. The results showed that CFP performed excellent inhibiting effect for the corrosion of the MS.

Keywords: Kinetic parameters, Adsorption, Corrosion, SEM

1. INTRODUCTION

Corrosion is a fundamental process playing an important role in economics and safety, particularly for metals and alloys. Steel has found wide application in a broad spectrum of industries and machinery; however its tendency to corrosion. The corrosion of steel is a fundamental academic and industrial concern that has received a considerable amount of attention. Among several methods used in combating corrosion problems, the use of chemical inhibitors remains the most cost effective and practical method. Therefore, the development of corrosion inhibitors based on organic compounds

containing nitrogen, sulphur and oxygen atoms are of growing interest in the field of corrosion and industrial chemistry as corrosion poses serious problem to the service lifetime of alloys used in industry [1-5].

Many corrosion inhibitors used in aqueous heating and cooling systems are generally toxic and generate health hazards. This toxic property limits the field of their applications. However there is a great demand for nontoxic corrosion inhibitors. The development of new corrosion inhibitors of non-toxic type, which do not contain heavy metals and organic phosphates, remains very important [6-9].

Cefapirin is the commercial name of (7R)-8-oxo-3-((prop-1-en-2-yloxy) methyl)-7-(pyridine-4-ylthio) acetamido)-5-thia-1-azabicyclo [4, 2, 0] oct-2-ene-2-carboylic acid. It is a broad-spectrum first generation cephalosporin antibiotic. This paper reports the use of electrochemical impedance spectroscopy (EIS), potentiodynamic polarization, weight loss, scanning electron microscopy (SEM) and contact angle measurement to investigate the nature of adsorption of cefapirin (CFP) on mild steel surface. The structure of CFP is shown in Fig. 1.



Figure 1. Structure of cefapirin (CFP) molecule

2. EXPERIMENTAL

2.1. Inhibitor

Stock solution of CFP was made in 10:1 ratio of water: ethanol mixture to ensure solubility. This stock solution was used for all experimental purposes.

2.2. Mild steel sample

The chemical composition of the working electrode, a mild steel electrode was determined as (wt. %) C = 0.17, Mn = 0.46, Si = 0.26, S = 0.017, P = 0.019 and balance Fe. It was mechanically ground with 320, 400, 600, 800, 1000 and 1200 emery paper, washed in acetone and bidistilled water then dried and put into the cell.

2.3. Electrochemical measurements

A three-electrode cell consisting of carbon steel working electrode (WE), a platinum counter electrode (CE) and saturated calomel electrode (SCE) as a reference electrode, was used for electrochemical measurements. All experiments were performed in atmospheric condition without stirring. Prior to the electrochemical measurement, a stabilization period of 30 min was allowed, which was proved to be sufficient to attain a stable value of E_{corr} .

The EIS measurements were carried out in a frequency range from 100 kHz to 0.00001 kHz under potentiodynamic conditions, with amplitude of 10 mV peak-to peak, using AC signal at E_{corr} .

The potential value polarization curves were recorded in the potential range of -250 to +250 mV (SCE) with scan rate 1 mV s⁻¹. All potentials were measured against SCE.

2.4. Weight loss measurements

Weight loss experiments were done according to the method described previously [10]. Weight loss measurements were performed at 308 K for 3 h by immersing the mild steel coupons into acid solution (100 mL) without and with various amounts of inhibitors. After the elapsed time, the specimen were taken out, washed, dried and weighed accurately.

The inhibition efficiency (μ_{WL} %) and surface coverage (θ) was determined by using the following equations:

$$\mu_{\rm WL} \% = \frac{w_0 - w_{\rm i}}{w_0} \times 100 \tag{1}$$

$$\theta = \frac{w_0 - w_i}{w_0} \tag{2}$$

Where, w_0 and w_i are the weight loss value in the absence and presence of inhibitor.

2.5 Scanning electron microscopy (SEM)

The carbon steel specimens (size $1.0 \text{ cm} \times 1 \text{ cm} \times 0.025 \text{ cm}$) were abraded with emery paper (320 –1200 grade) then were washed with distilled water and acetone. After immersion in 1 M HCl without and with addition of 400 ppm of CFP at 308 K for 3 h, steel specimens were cleaned with distilled water; dried using a cold air blaster, and then the surface was investigated using a Jeol JSM-5400 (SEM).

2.6 Contact angle measurements (static sessile drop method)

For the measurements of the contact angle, the mild steel samples described above were used. Prior to any contact angle measurements, the mild steel coupons were carefully cleaned in order to remove surface contamination like grease, dust or organic traces that could influence contact angle measurements through surface pinning of the liquid drop and or contamination of the liquid when the latter is put into contact with the sample surface. Aqueous acid solutions with different concentrations of the CFP were prepared and the samples were then immersed into these solutions for 3 h. Upon removal from the solutions, the samples were dried by means of gently nitrogen flow. Contact angle measurements were performed using the static sessile drop method with a Ramé-Hart goniometer (Netcong, USA).

3. RESULTS AND DISCUSSION

3.1 Electrochemical impedance spectroscopy

Impedance method provides information about the kinetics of the electrode processes and simultaneously about the surface properties of the investigated systems.



Figure 2. (a) Nyquist plots, (b) Typical polarization curves for corrosion of mild steel in 1 M HCl in the absence and presence of different concentrations of CFP and (c) the electrochemical equivalent circuit used to fit the impedance measurements.

The shape of impedance gives mechanistic information. The method is widely used for investigation of corrosion inhibition processes [11]. Nyquist plots of mild steel in 1 M HCl solution in the absence and presence of different concentrations of CFP are presented in Fig. 2a. It follows from Fig. 2a that a high frequency (HF) depressed charge-transfer semicircle was observed followed by a well defined inductive loop in the low frequency (LF) regions. The HF semicircle is attributed to the time constant of charge transfer and double-layer capacitance [12, 13]. The LF inductive loop may be attributed to the relaxation process obtained by adsorption species as Cl_{ads}^{-} and H_{ads}^{+} on the electrode surface [14].

To get more accurate fit of these experimental data, the measured impedance data were analysed by fitting in to equivalent circuit given in Fig. 2c. The equivalent circuit consists of the double-layer capacitance (C_{dl}) in parallel to the charge transfer resistance (R_{ct}), which is in series to the parallel of inductive elements (L) and R_L . The presence of L in the impedance spectra in the presence of the inhibitor indicates that mild steel is still dissolved by the direct charge transfer at the CFP-adsorbed mild steel surface [15].

Table 1. Electrochemical parameters derived from EIS and potentiodynamic polarization for mild steel in absence and presence of different concentrations of CFP

Inhibitor conc. (ppm)	R _s (Ω cm ²)	$Q (10^{-6} \times \Omega^{-1} \text{ s}^{\text{n}} \text{ cm}^{-2})$	n	L (H)	$R_{\rm ct}(\Omega \ { m cm}^2)$	$R_{\rm L}(\Omega \ { m cm}^2)$	$\mu_{ m R_{ct}}$ %	-E _{corr} (mV vs. SCE)	i _{corr} (μA cm ⁻²)	b _a (mV dec ⁻¹)	<i>b</i> _c (mV dec ⁻¹)	$\mu_{ m p}$ %
-	1.3	164	0.811	13	16	1	-	469	730	73	127	-
100	0.6	87	0.856	52	65	9	75	475	180	67	164	75
200	1.0	55	0.894	1	117	2	86	489	100	69	162	86
300	1.2	51	0.885	2	158	2	90	492	75	70	145	89
400	0.9	82	0.787	76	299	35	95	484	43	72	152	94

One constant phase element (CPE) is substituted for the capacitive element to give a more accurate fit, as the obtained capacitive loop is a depressed semi-circle. The depression in Nyquist semicircles is a feature for solid electrodes and often referred to as frequency dispersion and attributed to the roughness and other inhomogenities of the solid electrode [16]. The CPE is a special element whose admittance value is a function of the angular frequency (ω), and whose phase is independent of the frequency. The admittance and impedance of CPE is given by;

$$Y_{\rm CPE} = Y_0(i\omega)^n \tag{3}$$

where, Y_0 is the magnitude of CPE, *i* is an imaginary number $(i^2 = -1)$ and $n = \alpha / (\pi/2)$ in which α is the phase angle of CPE.

The point of intersection between the inductive loop and the real axis represents ($R_s + R_{ct}$). The electrochemical parameters, including R_s , R_{ct} , R_L , L, Y_0 and n, obtained from fitting the recorded EIS

using the electrochemical circuit of Fig. 2c are listed in Table 1. C_{dl} values derived from CPE parameters according to equation (4) are listed in Table 1.

$$C_{\rm dl} = Y_0 (\omega_{\rm max})^{\rm n-1} \tag{4}$$

where, ω_{max} is angular frequency ($\omega_{\text{max}} = 2\pi f_{\text{max}}$) at which the imaginary part of impedance (- Z_i) is maximal and f_{max} is AC frequency at maximum.

3.2 Potentiodynamic polarization measurements

Polarization measurements were carried out in order to gain knowledge concerning the kinetics of the cathodic and anodic reactions. Fig.2a shows the results of the effect of CFP concentration on the cathodic and anodic polarization curves of mild steel in 1 M HCl, respectively. It could be observed that both the cathodic and anodic reactions were suppressed with the addition of CFP, which suggested that the CFP reduced anodic dissolution and also retarded the hydrogen evolution reaction.

Electrochemical corrosion kinetics parameters, i.e. corrosion potential (E_{corr}), cathodic and anodic Tafel slopes (b_a , b_c) and corrosion current density (i_{corr}) obtained from the extrapolation of the polarization curves, were given in Table 1.

Table 2. Electrochemical parameter	rs derived from EIS	and potentiodynam	ic polarization	for mild steel
in absence and presence of c	lifferent concentration	ons of CFP		

Inhibitor concentration (ppm)	$E_{\rm a}$ (kJ mol ⁻¹)	$\lambda \text{ (mmy}^{-1}\text{)}$	$\Delta H^* (\mathrm{kJ} \mathrm{mol}^{-1})$	$\Delta S^* (\mathbf{J} \mathbf{K}^{-1} \operatorname{mol}^{-1})$
-	42.21	5.3×10^{8}	39.55	-86.75
400	73.69	5.2×10^{12}	71.04	-10.35

Fig. 2b represents the potentiodynamic polarization curves of mild steel in 1M HCl in the absence and presence of various concentrations of the CFP. It can be seen from the Fig. 2b that, in the presence of inhibitor, the curves are shifted to lower current regions, showing the inhibition tendency of the CFP. There was no definite trend observed in the E_{corr} values in the presence of CFP. In the present study, shift in E_{corr} values is in the range of 20-22 mV suggested that CFP acted as mixed type of inhibitor [17, 18]. The values of various electrochemical parameters derived by Tafel polarization of all the inhibitors are given in Table 1. Investigation of Table 1 revealed that the values of b_a change slightly in the presence of CFP where as more pronounced change occurred in the values of b_c , indicating that both anodic and cathodic reactions are effected but the effect on the cathodic reaction is more prominent. Thus, CFP acted as mixed type, but predominantly cathodic inhibitor [19]. Increase in inhibition efficiencies with increasing concentration of CFP revealed that inhibition action is due to adsorption on steel surface and the adsorption is known to depend on the chemical structure of the inhibitors.

3.3 Weight loss measurements

3.3.1 Effect of inhibitor concentration

The variation of inhibition efficiency (μ_{WL} %) with inhibitor concentration is shown in Fig.3a. Better inhibition efficiency at higher concentration may be attributed to larger coverage of metal with inhibitor molecules.

3.3.2 Effect of acid concentration

The variation of inhibition efficiency (μ_{WL} %) with concentration of acid solution is shown in Fig.3b. It can be seen that CFP acted as an efficient inhibitor in the studied concentration range.

3.3.3 Effect of immersion time

Fig.3c showed the effect of immersion time (3-24 h) at 308 K on the inhibition efficiency of CFP at 400 ppm concentration. Fig.3c showed that CFP inhibits the corrosion of mild steel for all immersion times. The inhibition efficiency of CFP gradually increased first from 3 to 15 h and thereafter almost constant suggesting the formation of persistent film on the metal surface.

100 100 (a 95 98 96 $\mu_{\rm wL}^{\rm M}$ 94 92 74 90∟ 0.0 100 200 300 400 500 0.5 2.0 1.0 C 1.5 2.5 $C_{\rm inh}(\rm ppm)$ (MI) 100 100 (c) 96 $\mu_{\rm wL}^{0.0}$ 92 88 Q, 84 18 21 24 310 320 330 3 12 15 27 340 6 *t*(h) $T(\mathbf{K})$

3.3.4 Effect of temperature

Figure 3. Variation of inhibition efficiency obtained from weight loss measurements with (a) concentration of CFP, (b) acid concentration (c) immersion time and (d) temperature of solution

The values of inhibition efficiencies obtained from weight loss measurement for the optimum concentration of CFP (400 ppm) in 1 M HCl are shown in Fig.3d. The inhibition efficiency of CFP decreased gradually with increasing temperature.

3.3.5 Thermodynamic activation parameters

The dependence of corrosion rate on temperature can be expressed by the Arrhenius equation and transition state equation [20, 21]:

$$\log(C_{\rm R}) = \frac{-E_{\rm a}}{2.303RT} + \log\lambda \tag{5}$$

$$C_{\rm R} = \frac{RT}{Nh} \exp\left(\frac{\Delta S^*}{R}\right) \exp\left(-\frac{\Delta H^*}{RT}\right)$$
(6)

where E_a apparent activation energy, λ the pre-exponential factor, ΔH^* the apparent enthalpy of activation, ΔS^* the apparent entropy of activation, h Planck's constant and N the Avogadro number, respectively. The apparent activation energy and pre-exponential factors at 400 ppm concentration of CFP can be calculated by linear regression between $\log C_R$ and 1/T (Table 2). All the linear regression coefficients are close to 1, indicating that corrosion of mild steel in hydrochloric acid can be explained using the kinetic model.



Figure 4. Arrhenius plots in absence and presence of 400 ppm concentration of CFP for (a) log C_R versus 1/T and (b) log (C_R/T) versus 1/T

Fig. 4a depicted an Arrhenius plot for mild steel immersed in 1 M HCl in the absence and presence of 400 ppm CFP. The plots obtained are straight lines and the slope of each straight line gives its apparent activation energy. Table 2 summarized E_a value for a 400 ppm CFP. Inspection of Table 2 showed that apparent activation energy increased in presence of CFP.

According to equation [5], corrosion rate (C_R) is being effected by both E_a and λ . In general, the influence of E_a on the mild steel corrosion was higher than that of λ on the mild steel corrosion. However, if the variation in λ was drastically higher than that of E_a , the value of λ might be the dominant factor to determine the mild steel corrosion. In the present case, E_a and λ decreased in the presence of inhibitor (the higher E_a and lower λ led to lower corrosion rate). Hence, it is clear that increment of E_a is the decisive factor affecting the corrosion rate of mild steel in 1 M HCl.

The relationship between $\log(C_{\rm R}/T)$ and 1/T is shown in Fig. 4b. The value of ΔH^* and ΔS^* were calculated and presented in Table 2. The positive sign of enthalpy reflect the endothermic nature of steel dissolution process meaning that dissolution of steel is difficult [22].

On comparing the values of the entropy of activation (ΔS^*) given in Table 2, it is clear that entropy of activation increased in the presence of CFP than in the absence of inhibitor. The increment of ΔS^* reveals that increase in disordering takes place on going from reactant to the activated complex [23].

3.3.6 Adsorption isotherm

The adsorption on the corroding surfaces never reaches the real equilibrium and tends to reach an adsorption steady state. When corrosion rate is sufficiently decreased in the presence of inhibitor, the adsorption steady state has a tendency to attain quasi-equilibrium state. Now, it is reasonable to consider quasi-equilibrium adsorption in thermodynamics using the appropriate adsorption isotherm. The degree of surface coverage (θ) for the inhibitor was obtained from average weight loss data. Different adsorption isotherms were tested in order to find the best fitted adsorption isotherm for adsorption of CFP on the surface of mild steel from 1 M HCl solution. Since, the linear regression coefficient of Langmuir adsorption isotherm is found more close to unity hence, was found best fit. With regard to the Langmuir adsorption isotherm, the surface coverage (θ) of the inhibitor on the mild steel surface is related to the concentration (C_{inh}) of the inhibitor in the bulk of the solution according to the following equation:

$$\theta = \frac{K_{\text{ads}} C_{\text{inh}}}{1 + K_{\text{ads}} C_{\text{inh}}} \tag{7}$$

where, K_{ads} is the equilibrium constant for the adsorption/desorption process. This equation can be rearranged to

$$\frac{C_{\rm inh}}{\theta} = \frac{1}{K_{\rm ads}} + C_{\rm inh} \tag{8}$$

It is a known fact that K_{ads} represents the strength between adsorbate and adsorbent. Large values of K_{ads} imply more efficient adsorption and hence better inhibition efficiency [24].

From the intercepts of the straight lines on the C_{inh}/θ -axis (Fig. 5a), K_{ads} can be calculated which is related to free energy of adsorption, ΔG_{ads}^{o} as given by equation 9.

$$\Delta G_{\rm ads}^{\rm o} = -RT\ln\left(55.5K_{\rm ads}\right) \tag{9}$$

The negative values of ΔG_{ads}^{o} ensure the spontaneity of the adsorption process and stability of the adsorbed film on the mild steel surface [1, 25]. It is usually accepted that the value of ΔG_{ads}^{o} around -20 kJ mol⁻¹ or lower indicates the electrostatic interaction between charged metal surface and charged organic molecules in the bulk of the solution while those around -40 kJ mol⁻¹ or higher involve charge sharing or charge transfer between the metal surface and organic molecules [26].



Figure 5. Adsorption isotherm plots for (a) Langmuir isotherm, (b) ln K_{ads} vs. 1/T, (c) ΔG_{ads}^{o} vs. T and (d) log ($\theta/1-\theta$) versus 1/T

Assuming thermodynamic model, corrosion inhibition of mild steel in the presence of CFP can be better explained, therefore, heat of adsorption and entropy of adsorption were calculated.

According to Van't Hoff equation [27, 28]:

$$\ln K_{\rm ads} = \frac{-\Delta H_{\rm ads}^{\rm o}}{RT} + \text{constant}$$
(10)

To calculate heat of adsorption $\ln K_{ads}$ was plotted against 1/T, as shown in Fig. 5b. The straight lines were obtained with slope equal to $(-\Delta H_{ads}^{\circ}/R)$ and intercept equal to $(\Delta S_{ads}^{\circ}/R + \ln 1/55.5)$. The calculated values of heat of adsorption and entropy of adsorption are listed in Table 3. Under the experimental conditions, the adsorption heat could be approximately regarded as the standard adsorption heat (ΔH_{ads}°) .

Table 3. Thermodynamic parameters for the adsorption of CFP on the mild steel at 400 ppm concentration.

Temperature	$\Delta G_{ m ads}^0$	Kads	$^{*}\Delta H_{ m ads}^{0}$	$^{*}\Delta S_{ m ads}^{0}$	$^{\dagger}\Delta H_{ m ads}^{0}$	$^{\dagger}\Delta S_{ m ads}^{0}$	$^{\dagger\dagger}\Delta H^{0}_{ m ads}$
(K)	(kJ mol ⁻¹)	$(\mathbf{M} \times 10^4)$	(kJ mol ⁻¹)	(J K ⁻¹ mol ⁻¹)	(kJ mol ⁻¹)	(J K⁻¹ mol⁻¹)	(kJ mol ⁻¹)
308	-35.78	2.42	-34.37	4.90	-34.21	5.70	5.70
318	-35.95	1.27					
328	-36.05	9.86	_				
338	-36.13	6.97	_				

The thermodynamic parameters ΔH_{ads}^{o} and ΔS_{ads}^{o} can also be calculated from the following equation:

$$\Delta G_{\rm ads}^{\rm o} = \Delta H_{\rm ads}^{\rm o} - T \Delta S_{\rm ads}^{\rm o} \tag{11}$$

A plot of ΔG_{ads}° vs. *T* gave straight line (Fig. 5c) with the slope equal to $-\Delta S_{ads}^{\circ}$, and the value of ΔH_{ads}° can be calculated from intercept.

An estimate of heat of adsorption was obtained for the trend of surface coverage with temperature as follows:

$$\log\left(\frac{\theta}{1-\theta}\right) = \log A + \log C_{\rm inh} - \left(\frac{\Delta H_{\rm ads}^{\rm o}}{2.303RT}\right)$$
(12)

A plot of $\log(\theta/1-\theta)$ versus 1/T is given in Fig. 5d. The slope $(-\Delta H_{ads}^{\circ}/2.303R)$ of the graph gives the value of heat of adsorption.

The values of ΔH_{ads}^{o} and ΔS_{ads}^{o} obtained by these different methods are in good agreement.

3.4 Scanning electron microscopy

The SEM images of mild steel surfaces are given in Fig. 6 a-c. The inspection of Fig. 6a, which is the micrograph of the mild steel surfaces exposed to 1 M HCl revealed that the specimen surface was strongly damaged in the absence of inhibitor. Fig. 6b showed the SEM image of the mild steel surface exposed to the 1 M HCl with the addition of 400 ppm CFP. There are no pits and cracks observed in the micrograph except polishing lines. The Fig. 6c showed polished mild steel surface.



Figure 6. (a) Scanning electron micrograph of mild steel surface exposed to free acid solution, (b) scanning electron micrograph of inhibited mild steel (1 M HCl + 400 ppm CFP) and (c) scanning electron micrographs of polished mild steel surface

3.5 Contact angle of acid solution on mild steel surface

Fig. 7 displays the contact angle, θ , as a function of CFP concentration for acid solutions on mild steel. For acid solution without inhibitor, contact angle, θ , is lowest (14.7) thereby metal showing most hydrophilic nature. By increasing contact angle, metal showed hydrophobic character to the acid solution containing inhibitor. The contact angle increased regularly with increasing concentration of inhibitor.



Figure 7. Contact angle, θ , of acid solutions containing different concentrations of CFP on mild steel surface

4. MECHANISM OF INHIBITION

It has been assumed that organic inhibitor molecule establish its inhibition action via the adsorption of the inhibitor onto the metal surface. The adsorption process is affected by the chemical structures of the inhibitors, the nature and charged surface of the metal and the distribution of charge over the whole inhibitor molecule. In general, owing to the complex nature of adsorption and inhibition of a given inhibitor, it is impossible for single adsorption mode between inhibitor and metal surface.

The adsorption and inhibition effect of CFP in HCl solution can be explained as follows: CFP might be protonated in the acid solution as follows:

$$CFP+xH^+ \leftrightarrow [CFPH_x]^{x+}$$
(13)

Thus, in aqueous acidic solutions, the CFP exists either as neutral molecules or in the form of cations (protonated CFP). Generally, two modes of adsorption could be considered. The neutral CFP may be adsorbed on the metal surface via the chemisorption mechanism, involving the displacement of water molecules from the metal surface and the sharing of electrons between the N atoms and iron. The CFP molecules can be also adsorbed on the metal surface on the basis of donor–acceptor interactions between π -electrons of nitrile group and carbonyl group and vacant d-orbital of iron. The d π - d π bonds are also formed by the overlap of 3d-electrons of Fe-atom to vacant 3d-orbital of S-atom. In another hand, it is well known that the steel surface has positive charge in acid solution [29], so it is difficult for the protonated CFP to approach the positively charged steel surface (H₃O⁺/metal interface) due to the electrostatic repulsion. Since chloride ions have a smaller degree of hydration, being specifically adsorbed, they create an excess negative charge towards the solution and favour more adsorption of the cations [1], the protonated CFP may adsorb through electrostatic interactions between the positively charged molecules and the negatively charged metal surface.

5. CONCLUSIONS

(a) CFP was found to be a good inhibitor for mild steel corrosion in acid medium.

(b) The inhibition efficiency of CFP decreased with temperature, which leads to an increase in activation energy of the corrosion process.

(c) EIS results were interpreted using an equivalent circuit in which a constant phase element (*CPE*) including an inductive element (*L*) was used in order to give more accurate fit to the experimental results.

(d) Potentiodynamic polarization curves revealed that CFP is a mixed-type inhibitor.

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