Conductometric Study of Potassium Chloride in Ethanol -Water Mixtures

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The molar conductivities of dilute solutions of potassium chloride in binary mixtures of ethanol and water were measured in the temperature range from 288.15 to 308.15 K at 5 K intervals. The experimental data were treated by the Lee-Wheaton conductivity equation and parameters Λ_0 and K_A derived. The ionic limiting molar conductivities (λ_0) were obtained using the literature values of the cation limiting transference number $t_0(K^+)$ from the same temperature range. The ionic Walden product $\lambda_0 \eta$, thermodynamic quantities for the ion-association reaction (ΔG^0 , ΔH^0 and ΔS^0) and the activation enthalpy of the ionic movement ΔH_i^* were calculated and discussed in terms of the ionic size, as well as solvent viscosity, permittivity, structure and basicity.

Keywords: ethanol - water mixtures, potassium chloride, limiting ionic conductivity, association to ion-pairs, thermodynamic quantities

1. INTRODUCTION

Studies of electrolytic conductance provide very important information concerning ions in solution. Mixed solvents are suitable for such studies because even a small change in solvent composition may lead to a significant difference in behaviour of the dissolved electrolyte. The formation of pairs and higher aggregates of oppositely charged ions occurs in a medium of low relative electrical permittivity. Conductivity measurements should cover a wider temperature range to make thermodynamics of these processes better understood.

In our previous works [1-7] the ion-pair association of alkali bromides in binary mixtures of water with two isomeric butanols was studied at five temperatures from 288.15 K to 308.15 K. The

systems water - ethanol - KCl were investigated conductometrically [8] at 283.15 K (only three waterrich systems) and 298.15 K (the whole composition range).

The present work reports conductometric data for the low concentration potassium chloride solutions in ethanol - water mixtures with alcohol mole fraction $x_{\rm E} = 0.05$, 0.10, 0.20, 0.40 and 0.60 at 288.15, 293.15, 298.15, 303.15 and 308.15 K. Data were processed by the Lee-Wheaton conductivity model with the distance parameter *R* fixed at R = a + s (where *a* represents the sum of ionic radii and *s* is the length of a water molecule) and two parameters, the limiting molar conductivity (Λ_0) and the association constant (K_A), were derived. Limiting transference numbers of KCl (t_0 at 298.15 K [9]) and their change with temperature [10] enabled the splitting of Λ_0 into ionic contributions (λ_0). The ionic conductivity λ_0 and its temperature dependence served to calculate the ionic Walden product $\lambda_0 \eta$ and Eyring's enthalpy of activation of ionic movement (ΔH_i^*).

An insight into the ion-association thermodynamics can still be get from the equilibrium constant K_A , though they are slight and wobbling with temperature.

2. EXPERIMENTAL

2.1. Reagents and chemicals

Water was distilled twice (specific conductivity $\approx 10^{-6}$ S cm⁻¹) and KCl (Merck, suprapur) was dried for six hours at 393.15 K before use. Ethanol (Merck, absolute, 99.8 %) was used without further purification. Solvent mixtures and the concentrated stock solutions were prepared by weight. The test solution concentration range was covered by adding stock to solvent. The maximum tested concentration was limited by the condition that no triple ions should appear [11]. Molarity ($c / \text{mol dm}^-$ ³) was determined as

$$c = \frac{dm}{1 + mM} \tag{1}$$

where *m* is molality (moles of electrolyte per kilogram of solvent), $d / \text{kg dm}^{-3}$ is the solution density and *M* the molar mass of electrolyte (0.07455 kg mol⁻¹ for KCl). By assuming a linear dependence of the solution density upon its molality,

 $d = d_0 + Dm \tag{2}$

(d_o is the solvent density), the density gradient $D / \text{kg}^2 \text{ dm}^{-3} \text{ mol}^{-1}$ was obtained. Its values at 293.15 K for the alcohol mole fraction (x_E) of 0.05, 0.10, 0.20, 0.40 and 0.60 amount to 0.0463, 0.0492, 0.0437, 0.0415 and 0.0511, respectively, and are assumed to be independent on temperature [12]. The relative error in molarity and solvent composition was about \pm 0.1 %.

2.2. Apparatus

The stock solution density at 293.15 K, as well as the densities of ethanol - water mixtures at all working temperatures, were determined by a digital density meter Anton Paar (model DMA 4500 M) with the uncertainty of ± 0.00005 kg dm⁻³.

The viscosity of ethanol - water mixtures was measured at each temperature using an Ostwald viscometer. The uncertainty in measurements of time was about ± 0.1 %.

Measurement of resistance by a component analyser Wayne - Kerr (model 6430 A) was described earlier in detail [6].

3. RESULTS AND DISCUSSION

3.1. Solvent properties and solution conductivity

The density and viscosity of ethanol - water mixtures were already reported at 293.15, 298.15 and 303.15 K [13]. Still, Table 1 contains only our new values.

The relative permittivity of the pure solvent was obtained by interpolation from literature data [14].

Molar conductivity of potassium chloride is given in Table 2.

	288.15 K	293.15 K	298.15 K	303.15 K	308.15 K
$x_{\rm E} = 0.05$					
$d_{\rm o}/{\rm kg}{\rm dm}^{-3}$	0.98059	0.97931	0.97776	0.97597	0.97392
η / mPa s	1.907	1.597	1.373	1.194	1.054
<i>E</i> r	75.25	73.50	71.72	70.03	68.32
$x_{\rm E} = 0.10$					
$d_{\rm o}/{\rm kg}{\rm dm}^{-3}$	0.96764	0.96535	0.96299	0.96048	0.95791
η / mPa s	2.728	2.239	1.866	1.596	1.375
<i>E</i> r	68.60	67.40	65.74	64.11	62.60
$x_{\rm E} = 0.20$					
$d_{\rm o}/{\rm kg}{\rm dm}^{-3}$	0.94076	0.93715	0.93352	0.92979	0.92597
η / mPa s	3.515	2.866	2.373	2.007	1.706
<i>E</i> r	58.62	57.11	55.61	54.20	52.81
$x_{\rm E} = 0.40$					
$d_{\rm o}/{\rm kg}{\rm dm}^{-3}$	0.88851	0.88438	0.88020	0.87595	0.87165
η / mPa s	3.070	2.569	2.179	1.882	1.634
<i>E</i> r	44.25	42.85	41.80	40.55	39.40
$x_{\rm E} = 0.60$					
$d_{\rm o}/{\rm kg}{\rm dm}^{-3}$	0.84936	0.84508	0.84075	0.83636	0.83197
η / mPa s	2.372	2.057	1.786	1.574	1.392
<i>E</i> r	35.33	34.25	33.20	32.20	31.18

 $^{a}x_{\rm E}$ is the mole fraction of ethanol in the mixture.

Table 2. Molar conductivity (Λ / S cm² mol⁻¹) of KCl in aqueous ethanol (x_E) at different concentrations (c / mol dm⁻³) and temperatures

	293.15 K		298. <u>15 K</u>		30 <u>3.15 K</u>		3 <u>08.15 H</u>	K
Λ	$10^{4} c$	Λ	$10^{4} c$	Λ	$10^{4} c$	Λ	$10^{4} c$	Λ
								123.848
								123.085
								121.987
								121.490
								121.245
								120.880
								120.407
								120.017
								119.709
					105.80	107.716	105.74	119.385
73.831	108.08	83.751	96.128	97.381				
56.064	43.083	63.965	10.283	75.847	51.098	84,792	27.214	97.839
								97.235
								96.786
								96.345
								95.918
								95.545
								95.237
								94.917
					100170	001002		94.566
								94.287
								94.003
				71.982				
39.746	7.4406	47.268	7.5826	55.512	16.919	64.433	8.2714	74.525
39.250	15.113	46.676	23.072	54.315	25.392	63.814	17.091	73.568
38.914	22.809	46.254	30.744	53.897	33.722	63.387	25.745	72.889
								72.353
								71.944
								71.571
								71.371
								70.897
								70.517
								70.242
			92.504	51.920				70.011
					101.30	61.135		69.899
37.150	92.181	44.161					100.71	69.708
31.617	7.6959	38.113	7.3843	43.792	15.887	49.779	7.5573	58.066
	76.162 75.804 75.582 75.300 75.301 75.302 74.798 74.610 74.398 74.176 73.815 73.815 73.815 55.425 55.114 54.767 54.390 54.150 53.296 53.297 53.079 52.938 39.746 39.250 38.316 38.580 38.376 38.168 37.968 37.959 37.359 37.359	Λ $10^4 c$ 76.162 28.198 75.804 36.777 75.582 44.955 75.300 53.513 75.037 61.442 74.798 69.248 74.610 77.246 74.398 85.176 74.176 92.687 73.815 100.32 73.815 100.32 73.815 100.32 73.815 108.08 55.425 51.172 55.114 59.138 54.767 66.924 54.390 74.503 54.150 81.809 53.921 89.394 53.693 96.557 53.468 103.826 53.237 53.079 52.938 30.327 38.76 7.4406 39.746 7.4406 39.756 52.083 37.810 59.303 37.651 66.148 37.539 79.258 37.239 86.020	Λ $10^4 c$ Λ 76.16228.19886.34275.80436.77785.96675.58244.95585.64075.30053.51385.31675.03761.44285.00374.79869.24884.79474.61077.24684.53674.39885.17684.36474.17692.68784.13273.815100.3283.94573.831108.0883.75156.06443.08363.96555.42551.17263.70155.11459.13863.46454.76766.92463.26354.39074.50363.06454.15081.80962.89953.92189.39462.74453.69396.55762.57453.468103.82662.46953.23753.07952.93839.7467.440647.26839.25015.11346.67638.91422.80946.25438.58030.32745.89538.37637.64145.60738.16844.94745.35437.96852.08345.11237.81059.30344.90737.65166.14844.72737.51572.62144.56937.23986.02044.283	A $10^4 c$ A $10^4 c$ 76.162 28.198 86.342 9.5743 75.804 36.777 85.966 18.295 75.582 44.955 85.640 27.560 75.300 53.513 85.316 36.826 75.037 61.442 85.003 44.269 74.798 69.248 84.794 59.624 74.610 77.246 84.536 67.285 74.398 85.176 84.364 74.628 74.176 92.687 84.132 82.134 73.815 100.32 83.945 88.987 73.831 108.08 83.751 96.128 55.425 51.172 63.701 19.089 55.114 59.138 63.464 27.879 54.767 66.924 63.263 36.902 54.390 74.503 63.064 45.273 54.150 81.809 62.899 53.588 53.921 89.394 62.744 61.541 53.693 96.557 62.574 69.626 53.468 103.826 62.469 77.375 53.296 85.983 53.237 93.589 53.079 101.18 52.938 108.51 39.746 7.4406 47.268 7.5826 39.250 15.113 46.676 23.072 38.914 22.809 46.254 30.744 38.580 30.327 45.895 38.141 38.376 37.641 4	Λ $10^4 c$ Λ $10^4 c$ Λ 76.162 28.198 86.342 9.5743 101.881 75.804 36.777 85.966 18.295 101.068 75.582 44.955 85.640 27.560 100.419 75.300 53.513 85.316 36.826 99.772 75.037 61.442 85.003 44.269 99.413 74.798 69.248 84.794 59.624 98.763 74.610 77.246 84.364 74.628 98.161 74.176 92.687 84.132 82.134 97.874 73.815 100.32 83.945 88.987 97.666 73.831 108.08 83.751 96.128 97.381 55.425 51.172 63.701 19.089 75.188 55.142 51.172 63.701 19.089 75.188 54.390 74.503 63.644 27.879 74.706 54.390 74.503 63.064 45.273 73.932 54.150 81.809 62.899 53.588 73.622 53.921 89.394 62.744 61.541 73.365 53.237 93.589 72.390 71.982 53.237 93.589 72.390 53.693 96.557 62.574 69.626 73.921 85.983 72.586 53.237 93.589 72.390 53.693 96.557 62.5469 77.375 72.832 53.687 <	A $10^4 c$ A $10^4 c$ A $10^4 c$ 76.16228.19886.3429.5743101.88136.09175.80436.77785.96618.295101.06844.62975.58244.95585.64027.560100.41952.61175.30361.44285.00344.26999.71368.64674.79869.24884.79459.62498.76376.36474.61077.24684.53667.28598.45784.04774.39885.17684.36474.62897.87498.67773.815100.3283.94588.98797.866105.8073.815100.3283.94588.98797.866105.8073.831108.0883.75196.12897.381101.58055.42551.17263.70119.08975.18859.00255.11459.13863.26336.90274.28675.43154.39074.50363.06445.27373.93288.13154.39074.50363.06445.27373.93288.13154.39074.50362.24973.35572.84675.43153.92189.39462.74461.54173.36599.51253.69396.55762.57469.62673.100106.7653.468103.82662.46977.37572.83253.92153.079101.11872.18052.39233.7193.58972.39053.07457.84757	$\begin{array}{c ccccccccccccccccccccccccccccccccccc$	$\begin{array}{c c c c c c c c c c c c c c c c c c c $

84.227	26.671	84.291	30.392					81.949	43.536
78.383	26.875	78.412	30.626	83.100	34.237			76.465	43.895
72.534	27.092	72.598	30.883	76.929	34.522	77.993	38.802	70.826	44.266
66.457	27.336	66.488	31.172	70.643	34.843	71.617	39.168	64.807	44.726
60.325	27.593	60.298	31.486	64.202	35.183	65.046	39.577	58.943	45.184
54.180	27.882	54.005	31.828	57.597	35.563	58.250	40.036	52.974	45.683
47.790	28.196	47.728	32.203	50.906	35.989	51.497	40.527	46.974	46.235
41.345	28.545	41.147	32.631	44.187	36.457	44.778	41.085	40.700	46.893
34.736	28.947	34.441	33.119	37.217	36.999	37.612	41.705	34.311	47.530
27.899	29.418	28.068	33.649	29.945	37.653	30.189	42.478	27.588	48.426
20.963	29.966	21.433	34.309	22.729	38.383	22.895	43.318	21.064	49.312
13.966	30.648	14.464	35.119	15.368	39.311	15.101	44.441	13.988	50.604
6.8141	31.571	7.1942	36.252	7.2441	40.655	7.1279	46.021	6.4895	52.477
<i>x</i> _E =0.60									
		94.815	34.321	95.405	39.006			94.201	51.589
		88.775	34.507	88.536	39.204	95.170	45.248	87.781	51.843
		82.012	34.705	81.819	39.424	88.533	45.475	81.162	52.119
95.188	29.445	75.275	34.896	74.978	39.663	81.897	45.745	74.459	52.409
88.531	29.588	68.578	35.105	68.125	39.917	75.060	46.020	67.606	52.833
81.843	29.743	61.450	35.351	60.939	40.201	68.129	46.329	60.545	53.171
74.903	29.914	54.150	35.619	53.558	40.520	60.909	46.668	53.431	53.667
68.134	30.0920	46.852	35.905	46.253	40.868	53.850	47.033	46.115	54.146
53.829	30.238	39.213	36.247	38.811	41.264	46.465	47.447	38.641	54.650
46.580	30.479	31.694	36.263	31.227	41.678	39.057	47.893	31.111	55.262
39.109	30.752	23.954	36.710	23.423	42.212	31.493	48.420	23.336	55.984

3.2. Model and data processing

The limiting molar conductivity Λ_0 and association constant K_A were determined using a chemical model of conductivity based on the Lee-Wheaton equation [15] in the Pethybridge and Taba version [16], LWPT,

$$\Lambda_{c\alpha} = \Lambda_0 \left[1 + C_1 \beta \kappa + C_2 (\beta \kappa)^2 + C_3 (\beta \kappa)^3 \right] - \frac{\rho \kappa}{1 + \kappa R} \left[1 + C_4 \beta \kappa + C_5 (\beta \kappa)^2 + \frac{\kappa R}{12} \right]$$
(3)

$$\rho = \frac{Fe}{3\pi\eta}, \qquad q = \frac{e^2}{8\pi\varepsilon_o\varepsilon_r kT}, \qquad \kappa^2 = 16\pi N_A q c \alpha, \qquad (4a,b,c)$$

 $\Lambda_{c\alpha}$ is the molar conductivity of free ions and Λ_0 the same quantity at infinite dilution, coefficients $C_1 - C_5$ are the functions of κR [16], R is the greatest centre-to-centre distance between ions in the ion-pair formed, κ is the Debye parameter, $\beta = 2q$ (q is the Bjerrum critical distance), e is the proton charge, ε_r relates the solvent permittivity to that of vacuum (ε_0); other symbols have their usual meaning.

Thermodynamic equilibrium constant $K_{A,c}$ (subscript *c* indicating the molarity scale) for the association reaction

$$K^{+} + Cl^{-} \rightleftharpoons K^{+} \cdot Cl^{-}$$

$$c\alpha \quad c\alpha \quad c(1-\alpha)$$
(5)

is given by the expression

$$K_{\mathrm{A},c} = \frac{c^{\circ}(1-\alpha)}{c\alpha^2 y_{\pm}^2} \tag{6}$$

where $c^{\circ} = 1 \mod dm^{-3}$, $c\alpha$ and $c(1-\alpha)$ are the equilibrium concentrations of the fraction of free ions and ion pairs, respectively; α is the degree of dissociation represented by the ratio of the stoichiometric molar conductivity to that of free ions,

$$\alpha = \frac{\Lambda}{\Lambda_{c\alpha}} \tag{7}$$

The mean activity coefficient of the free ions is given by the relationship:

$$y_{\pm} = e^{\frac{-\kappa q}{1+\kappa R}} \tag{8}$$

The chemical model is obtained by combining equations (6) and (7),

$$\Lambda = \frac{c^{\circ} \Lambda_{c\alpha}}{c^{\circ} + K_{A,c} c \alpha y_{\pm}^{2}}$$
⁽⁹⁾

With the numerator described by some theoretical equation, in this case (3), the chemical model becomes a function of concentration and three adjustable parameters:

$$\Lambda = f(c; \Lambda_0, K_{\mathrm{A},c}, R) \tag{10}$$

The model was resolved by an iterative procedure: parameters Λ_0 and $K_{A,c}$ were adjusted according to Beronius [17] for each selected value of *R* until the standard deviation (σ) of experimental conductivities from the calculated ones,

$$\sigma^2 = \frac{\sum (\Lambda_{\text{calc}} - \Lambda_{\text{exp}})^2}{n-3} \tag{11}$$

would have achieved its minimal value (*n* is the number of solutions tested in one run). The values of parameters Λ_0 and $K_{A,c}$ so derived change uniformly with temperature, while the distance parameter *R* covers a wide range of values, showing irregular trend with temperature (no significant minima in the plot $\sigma - R$ was obtained for any solvent composition). The experimental data were therefore processed by a two-parameter fit, $\Lambda = f(c; \Lambda_0, K_{A,c})$, *i.e. R* had to be chosen in accord with some of the existing criteria. A solvent separated ion-pair was used as a model with R = a + s; *a* represents the sum of radii of K⁺ and Cl⁻ (314 pm, according to Pauling [18]) and *s* for aqueous mixtures is the length of a water molecule, (280 pm [12]), which makes R = 594 pm. The values of Λ_0 and $K_{A,c}$ obtained by this condition, along with standard deviation σ of experimental Λ from the model (9), are listed in Table 3; numeral 3 in Eq. (11) was switched to 2. Standard deviations of Λ_0 and $K_{A,c}$ were estimated as suggested in the literature [19]. To avoid the influence of the solvent thermal expansion to the reaction enthalpy, $K_{A,c}$ was converted to the molality scale, $K_{A,m} = K_{A,c} d_0 / \text{kg dm}^{-3}$.

Fig. 1 shows the concentration dependence of the experimental molar conductivity (Λ_{exp}) for KCl at five temperatures in the ethanol ($x_E = 0.60$) - water mixture; full lines are drawn through points computed by the LWPT conductivity model (Λ_{calc}). Analogous plots for the other four mixtures are similar.

Table 3. Limiting molar conductivity (Λ_0), ion-association constants ($K_{A,c}$, $K_{A,m}$) and standard deviation (σ) of experimental Λ from the model LWPT (with *R* fixed at 594 pm) for KCl in ethanol (x_E) - water mixtures

<i>T</i> /K	$\Lambda_{\rm o}/{\rm S~cm^2~mol^{-1}}$	$K_{\mathrm{A},c}$	$K_{\mathrm{A},m}$	$\sigma/S \text{ cm}^2 \text{ mol}^{-1}$
		$x_{\rm E} = 0.05$		
288.15	78.78 ± 0.06	0.99 ± 0.13	0.97 ± 0.13	0.06
293.15	89.40 ± 0.02	0.80 ± 0.04	0.79 ± 0.04	0.02
298.15	104.03 ± 0.02	1.31 ± 0.04	1.28 ± 0.04	0.03
303.15	116.03 ± 0.03	1.80 ± 0.05	1.75 ± 0.05	0.03
308.15	128.59 ± 0.07	1.64 ± 0.10	1.60 ± 0.10	0.07
		$x_{\rm E} = 0.10$		
288.15	57.22 ± 0.04	2.56 ± 0.13	2.48 ± 0.13	0.05
293.15	66.95 ± 0.02	1.20 ± 0.05	1.16 ± 0.05	0.01
298.15	77.67 ± 0.01	1.58 ± 0.03	1.52 ± 0.03	0.02
303.15	89.36 ± 0.04	1.52 ± 0.08	1.46 ± 0.08	0.02
308.15	101.93 ± 0.03	2.12 ± 0.06	2.03 ± 0.06	0.03
		$x_{\rm E} = 0.20$		
288.15	40.70 ± 0.02	3.15 ± 0.10	2.96 ± 0.09	0.03
293.15	48.38 ± 0.03	3.57 ± 0.17	3.34 ± 0.16	0.05
298.15	56.84 ± 0.04	3.21 ± 0.16	3.00 ± 0.15	0.05
303.15	66.83 ± 0.05	2.36 ± 0.17	2.19 ± 0.16	0.06
308.15	76.52 ± 0.04	2.74 ± 0.12	2.54 ± 0.11	0.06
		$x_{\rm E} = 0.40$		
288.15	33.28 ± 0.06	3.11 ± 0.46	2.76 ± 0.41	0.06
293.15	39.58 ± 0.07	6.71 ± 0.49	5.94 ± 0.43	0.10
298.15	45.60 ± 0.02	9.55 ± 0.10	8.41 ± 0.09	0.02
303.15	53.02 ± 0.01	9.86 ±0.06	8.64 ± 0.05	0.01
308.15	60.65 ± 0.02	10.62 ± 0.11	9.26 ± 0.10	0.03
		$x_{\rm E} = 0.60$		
288.15	33.53 ±0.01	25.19 ± 0.04	21.40 ± 0.04	0.01
293.15	38.65 ± 0.02	28.65 ± 0.18	24.21 ± 0.15	0.02
298.15	43.42 ± 0.01	27.68 ± 0.08	23.27 ± 0.07	0.01
303.15	49.21 ± 0.01	29.69 ± 0.07	24.83 ± 0.06	0.01
308.15	55.98 ± 0.02	32.38 ± 0.18	26.94 ± 0.15	0.02

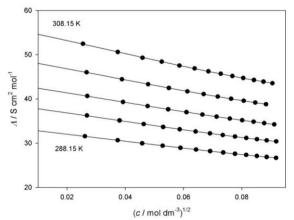


Figure 1. Molar conductivity of KCl in ethanol - water mixture with $x_E = 0.60$ from 288.15 K to 308.15 K: experimental data (•); values calculated by LWPT using Λ_0 and $K_{A,c}$ from Table 3 (lines).

In media of lower permittivity (ε_r) the interactions ion - dipole (shell 1) - dipoles (shell 2) are stronger and the hydrodynamic radii *r* of ions accordingly greater. Limiting molar conductivity is inversely proportional to the medium viscosity and moving-sphere radius, $\lambda_o \propto 1 / \eta r$, as derived from the Stokes model, meaning that opposite changes in η and ε_r should have the same influence on λ_o . Up to the ethanol mole fraction of 0.2 the increasing η and decreasing ε_r (Table 1) both contribute to the Λ_o descend which is therefore very steep (Table 3 and Fig. 2). From $x_E = 0.2$ on the relative decrease in permittivity is about twofold greater than that in viscosity, the effect of η is more than compensated by that of ε_r and Λ_o is slightly descending. With increasing temperature, on the other hand, the latter decrease is four to eight times greater than the former (Table 1) and Λ_o is ascending (Table 3).

Small constants of the ionic equilibria obtained conductometrically are not quite reliable. Still, barring two values, K_A is increasing with the ethanol content (Table 3) as expected – lower ε_r enhances the attraction of oppositely charged ions. Despite somewhat higher scatter with temperature a positive general trend in K_A is recognized, except for the structurally critical water-rich region (as indicated by the viscosity curve in Fig. 2) where it is undoubtedly negative.

3.3. Ionic limiting conductivity and Walden product

The cation limiting transference numbers for KCl in aqueous ethanol at 298.15 K [9] were chosen as points of reference. The temperature effect on those numbers in the ethanol ($x_E = 0.05, 0.10, 0.15, 0.20$ and 0.30) - water mixtures (expressed by slope of the straight line $\frac{\ln(1-t_+)}{t_+}$ against $\frac{1}{T}$ [10]) served to derive the $t_0(K^+)$ values at the remaining four temperatures (Table 4); those for $x_E = 0.4$ were obtained by extrapolation and probably are less accurate.

The limiting conductivities of K⁺ and Cl⁻ (Table 5) were determined by the relations $\lambda_0(K^+) = t_0(K^+)\Lambda_0(KCl)$ and $\lambda_0(Cl^-) = \Lambda_0(KCl) - \lambda_0(K^+)$, using data from Tables 3 and 4; corresponding water values were calculated through the parameters [20] of assumedly linear function $\lambda_0(T)$. Curves of their change with composition at 298.15 K and the curve for Λ_0 already discussed have the same shape (Fig. 2), since the transference numbers are always near 0.5.

Table 4. The cation limiting transference number for KCl in ethanol (x_E) - water mixtures from its temperature dependence [10] with respect to the value at 298.15 K [9]

				$x_{\rm E}$			
<i>T /</i> K	0.05	0.10	0.15	0.20	0.30	0.40	0.60
288.15	0.5084	0.5168	0.5134	0.5085	0.4938	0.4862^{b}	
293.15	0.5057	0.5125	0.5113	0.5063	0.4930	0.4861 ^b	
298.15 ^a	0.5031	0.5091	0.5087	0.5036	0.4915	0.4856	0.4883
303.15	0.5006	0.5063	0.5056	0.5003	0.4895	0.4846^{b}	
308.15	0.4982	0.5045	0.5021	0.4965	0.4868	0.4832 ^b	

^aLiterature data [9]; ^bextrapolated values

Table 5. The ionic limiting molar conductivity $\lambda_o / S \text{ cm}^2 \text{ mol}^{-1}$ in ethanol (x_E) - water mixtures at different temperatures

						x_{E}						
	0.00^{a}		0.05		0.10		0.20		0.40		0.60	
<i>T /</i> K	\mathbf{K}^+	Cl^{-}	\mathbf{K}^+	Cl	\mathbf{K}^+	Cl	\mathbf{K}^+	Cl	\mathbf{K}^+	Cl	\mathbf{K}^+	Cl⁻
288.15	60.4	61.3	40.05	38.73	29.57	27.65	20.70	20.00	16.18	17.10	-	-
293.15	67.4	68.3	45.21	44.19	34.31	32.64	24.49	23.88	19.24	20.34	-	-
298.15	74.4	75.4	52.33	51.69	39.54	38.13	28.63	28.22	22.15	23.46	21.20	22.22
303.15	81.4	82.5	58.09	57.95	45.24	44.12	33.44	33.40	25.69	27.33	-	-
308.15	88.4	89.6	64.06	64.52	51.43	50.51	37.99	38.53	29.31	31.34	-	-

^aFrom empirical straight lines $\lambda_0(T)$ [20]

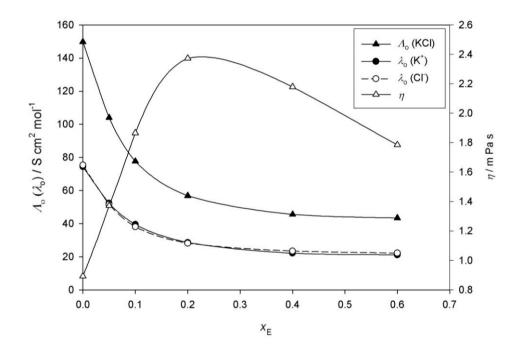


Figure 2. The dependence of the limiting molar conductivities ($\Lambda_0(\text{KCl})$, $\lambda_0(\text{K}^+)$, $\lambda_0(\text{Cl}^-)$ and viscosity on the ethanol mole fraction (x_E) in mixtures with water at 298.15 K.

The ionic Walden products $(\lambda_0 \eta)$ were obtained by multiplying each datum from Table 5 by the appropriate viscosity; values of η for mixtures were taken from Table 1, those for water in the temperature range 283.15 - 313.15 K [21a] were shown graphically and interpolated at 298.15 K and 308.15 K.

All results are listed in Table 6, but only those at 288.15, 298.15 and 308.15 K are presented against x_E in Fig. 3 in order to keep it transparent; barring few overlaps, the curves for 293.15 K and 303.15 K would lie between the previous ones and basically have their shape.

						$x_{\rm E}$						
	0.00^{a}		0.05		0.10		0.20		0.40		0.60	
<i>T /</i> K	\mathbf{K}^+	Cl	\mathbf{K}^+	Cl	\mathbf{K}^+	Cl	\mathbf{K}^+	Cl	\mathbf{K}^+	Cl	\mathbf{K}^+	Cl⁻
288.15	68.8	69.8	76.38	73.85	80.67	75.43	72.74	70.31	49.68	52.50	-	-
293.15	67.5	68.4	72.20	70.57	76.82	73.07	70.20	68.45	49.43	52.26	-	-
298.15	66.2	67.1	71.86	70.97	73.78	71.14	67.93	66.96	48.25	51.12	37.87	39.68
303.15	64.9	65.8	69.36	69.19	72.21	70.41	67.11	67.03	48.36	51.43	-	-
308.15	63.7	64.5	67.52	68.01	70.71	69.45	64.81	65.73	47.89	51.22	-	-
$\Delta W^{ m b}$	7.7	7.9	12.3	8.2	13.5	8.4	11.7	6.8	3.7	2.5	-	-
			1(O(W)	$-W_{\cdots}$							

^a
$$\eta$$
 from [21a]; ^b $\Delta W = \frac{100(W_{298} - W_{308})}{W_{298}}$

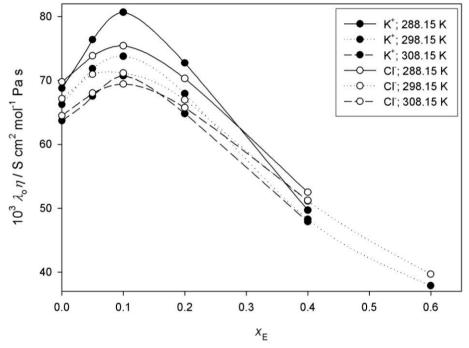


Figure 3. The ionic Walden products for KCl in dependence on the mole fraction of ethanol in aqueous mixture (x_E) at three temperatures.

An ion and the bulk-solvent are competing for molecules in the secondary shell (shell 2). In principle larger ion and the more developed bulk-structure make that shell thiner, and vice versa. In the region of the enhanced water structure the secondary shell contribution to the hydrodynamic radius *r* is the least and Walden product *W* exhibits a maximum (Fig. 3 observed earlier [7, 22, 23] as well); the temperature dependence of that contribution "modulates" the sum of the bare-ion radius and the primary shell width (shell 1, a monolayer of oriented molecules) but never making $r(K^+) > r$ (Cl⁻), for the $W(K^+)$ maximum is always exceeding that of Cl⁻. By further addition of ethanol the steadily decreasing ε_r and crumbling water structure both favour the broadening of shell 2, *r* is growing up and *W* is falling down, accordingly; the $W(Cl^-)$ decrease is less steep (Fig. 3) owing most likely to the

inductive effect of numerous ethyl-groups which is weakening H-bonds with anion by making the mixtures more basic [24].

The relative ε_r decrease with increasing temperature ($\Delta \varepsilon_r$) is about 10 % in all systems (Table 1), still the relative Walden product decrease (ΔW) is far away from constancy showing maximum at $x_E = 0.1$ (Table 6). Uniformed influence of $\Delta \varepsilon_r$ on ΔW is most likely modulated by the structural contribution [6]: a given quantity of heat will produce a greater disorder in a better organized bulk-structure, more molecules will be liberated and an ion will elongate its *r* to a greater extent by attracting them into its initially thiner shell 2.

The chloride ion is less sensitive to the effect described (Table 6) out of its lower surface charge density.

3.4. Thermodynamic quantities

The standard enthalpy of the association reaction (ΔH°) and the activation enthalpy of the charge transport (ΔH_{i}^{*}), both assumed as independent on temperature, were calculated by a least-squares treatment of the expressions,

$$\ln K^{\circ}_{A,m} = -\frac{\Delta H^{\circ}}{RT} + C \tag{12}$$

$$\ln(\lambda d^{2/3})_{o} = -\frac{\Delta H_{i}^{*}}{RT} + C'$$
(13)

using data for $K_{A,m}^{\circ}$ (Table 3) and λ_{\circ} (Table 5) at different *T*; density data for water and mixtures were taken from literature [21b] and Table 1, respectively. The standard deviation of each enthalpy was derived from the corresponding slope [25]. Four specially discrepant points, omitted in Fig.4, were excluded from data processing: at 288.15 K for x_E of 0.10 and 0.40, at 293.15 K for $x_E =$ 0.05, at 303.15 K for $x_E = 0.20$. For the mixture with $x_E = 0.100$ the rejected $K_{A,m}$ value was replaced by one recalculated by the LWPT model from the pairs (*c*, Λ) reported at 283.15 K [8]. The experimental points of Eq. (13) and "best" straight lines are shown in Fig. 5 for potassium ion.

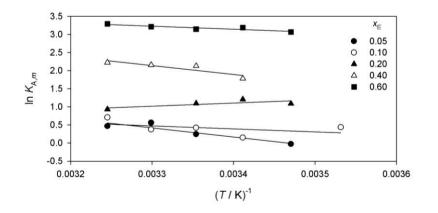


Figure 4. Plot of $\ln K_{A,m}$ against T^{-1} for KCl in ethanol (x_E) - water mixtures.

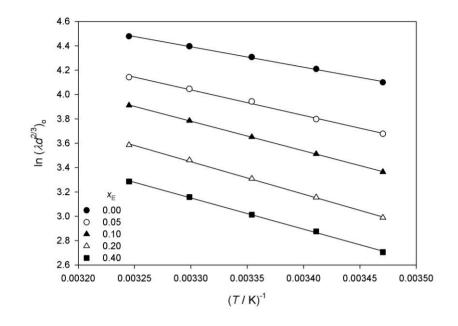


Figure 5. Plot of $\ln (\lambda d^{2/3})_0$ against T^{-1} for K⁺ in ethanol (x_E) - water mixtures.

The Gibbs energy and entropy changes (ΔG° and ΔS°), as well as their standard deviations, were computed as described before [4, 5]. All thermodynamic data for association are listed in Table 7 and presented graphically in Fig. 6 against $x_{\rm E}$.

Table 7. Thermodynamic	quantities for	or the association	n of ions K^+	and Cl ⁻	in ethanol $(x_{\rm E})$ - water
mixtures at 298.15 l	K				

$x_{\rm E}$	$\Delta G^{\circ}/ \text{ kJ mol}^{-1}$	$\Delta H^{\circ}/ \text{ kJ mol}^{-1}$	ΔS° / J K ⁻¹ mol ⁻¹
0.05	-0.6 ± 0.09	20.9 ± 6.0	72 ± 20
0.10	-1.0 ± 0.05	7.0 ± 7.6	27 ± 26
0.20	-2.7 ± 0.1	-7.2 ± 4.7	-15 ± 16
0.40	-5.3 ± 0.03	20.6 ± 7.5	87 ± 25
0.60	-7.8 ± 0.01	7.2 ± 1.9	50 ± 6

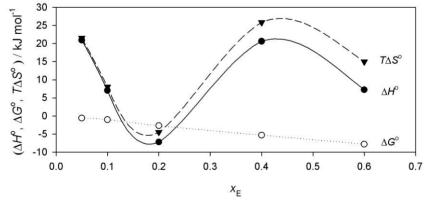


Figure 6. Thermodynamic quantities of the ion-association reaction for KCl in aqueous ethanol of mole fraction $x_{\rm E}$ at 298.15 K.

Unlike Gibbs energy, the enthalpy and entropy change reflects the structural changes accompanying the pairing of ions. In spite of an aggravating uncertainty in ΔH° and ΔS° the minimum in the structurally critical water-rich region is not a random occurence: the heat and order changes resulting from the break of shells around approaching ions compensate for those consorting the creation of solvent-separated pair and the building up of bulk-solvent.

The activation enthalpy of ionic movement is listed in Table 8 and its dependence on x_E presented in Fig.7.

Table 8. Activation enthalpy of ionic movement for K^+ , Cl^- and composite in ethanol (x_E) - water

mixtures in the temperature range from 288 K to 308 K

$x_{\rm E}$	$\Delta H^*_{\mathrm{K}^+}$ / kJ mol 1	$\Delta H^{*}_{ ext{Cl}^{-}}$ / kJ mol $^{ ext{-}1}$	ΔH^* / kJ mol ⁻¹
0.00	13.9 ± 0.3	13.9 ± 0.3	13.9 ± 0.3
0.05	17.4 ± 0.6	18.9 ± 0.6	18.2 ± 0.6
0.10	20.2 ± 0.1	22.0 ± 0.3	21.1 ± 0.2
0.20	22.2 ± 0.4	23.9 ± 0.3	23.0 ± 0.3
0.40	21.3 ± 0.4	21.8 ± 0.3	21.6 ± 0.4
0.60	-	-	18.2 ± 0.3

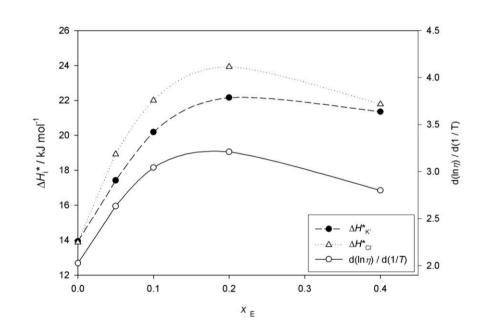


Figure 7. Activation enthalpy of the charge transport for K^+ and Cl^- and the temperature gradient of viscosity in aqueous ethanol of mole fraction x_E .

The ions K⁺ and Cl⁻ differ very slightly in that quantity, so the composite enthalpy (obtained through Λ_0 instead of λ_0) should have practically the same standard deviation [26]. The solvent flow and the ion migration are governed by similar transport mechanisms [12] as indicated by the shape of curves in Fig.7.

4. CONCLUSIONS

The present work reports conductometric data for the low concentration potassium chloride solutions in ethanol - water mixtures with alcohol mole fraction $x_{\rm E} = 0.05$, 0.10, 0.20, 0.40 and 0.60 in temperature range from 288.15 to 308.15 K. Molar conductivity decreases by increasing the proportion of ethanol in the mixture and increases with increasing temperature. In the region of the enhanced water structure the secondary shell contribution to the hydrodynamic radius of ions is the least and Walden product exhibits a maximum. ΔH° and ΔS° exhibit the minimum in the structurally critical water-rich region because the heat and order changes resulting from the break of shells around approaching ions compensate for those consorting the creation of solvent-separated pair and the

building up of bulk-solvent. The solvent flow and the ion migration are governed by similar transport mechanisms as indicated by the values of the activation enthalpy of the charge transport for K^+ and Cl^- and the temperature gradient of viscosity in aqueous ethanol mixtures.

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